

An Overview of U.S. DOE's Activities for Hydrogen Fuel Cell Technologies

U.S. DEPARTMENT OF **ENERGY** | Energy Efficiency & Renewable Energy



Materials Challenges in Alternative & Renewable Energy

Clearwater, Florida

2/27/2012

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Storage Team Lead

U.S. Department of Energy

Fuel Cell Technologies Program

The **mission** of the Hydrogen and Fuel Cells Program is to enable the widespread commercialization of hydrogen and fuel cell technologies through:

- basic and applied research
- technology development and demonstration
- addressing institutional and market challenges

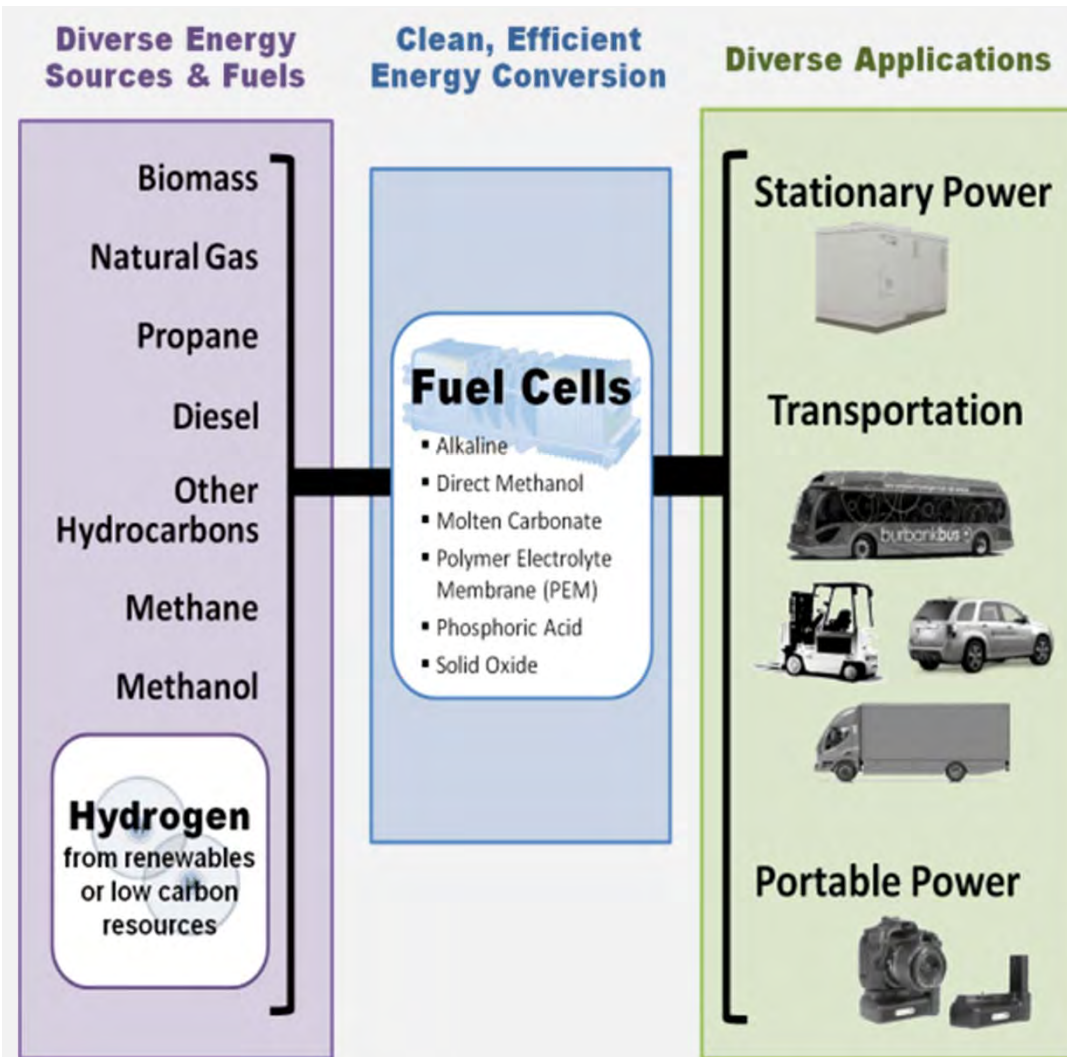
Achieving this mission will help reduce greenhouse gas emissions and oil consumption while advancing renewable energy.

Key Goals: Develop hydrogen and fuel cell technologies for:

1. **Early markets** (*e.g., stationary power, forklifts, portable power*)
2. **Mid-term markets** (*e.g., residential CHP, auxiliary power, buses and fleet vehicles*)
3. **Longer-term markets, 2015-2020** (*including mainstream transportation, with focus on passenger cars*)

The Role of Fuel Cells

Key Benefits



Very High Efficiency

- > 60% (electrical)
- > 70% (electrical, hybrid fuel cell / turbine)
- > 80% (with CHP)

Reduced CO₂ Emissions

- 35–50%+ reductions for CHP systems (>80% with biogas)
- 55–90% reductions for light-duty vehicles

Reduced Oil Use

- >95% reduction for FCEVs (vs. today's gasoline ICEVs)
- >80% reduction for FCEVs (vs. advanced PHEVs)

Reduced Air Pollution

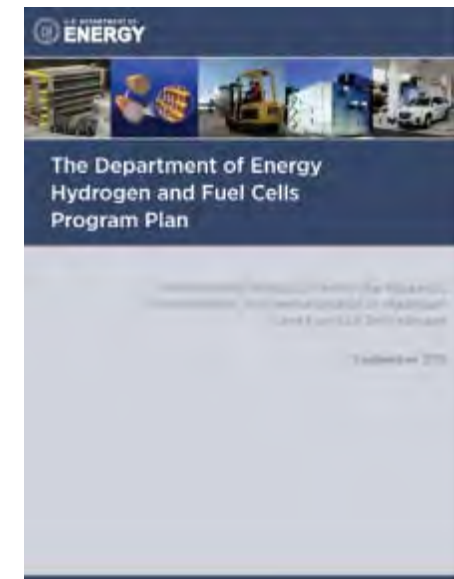
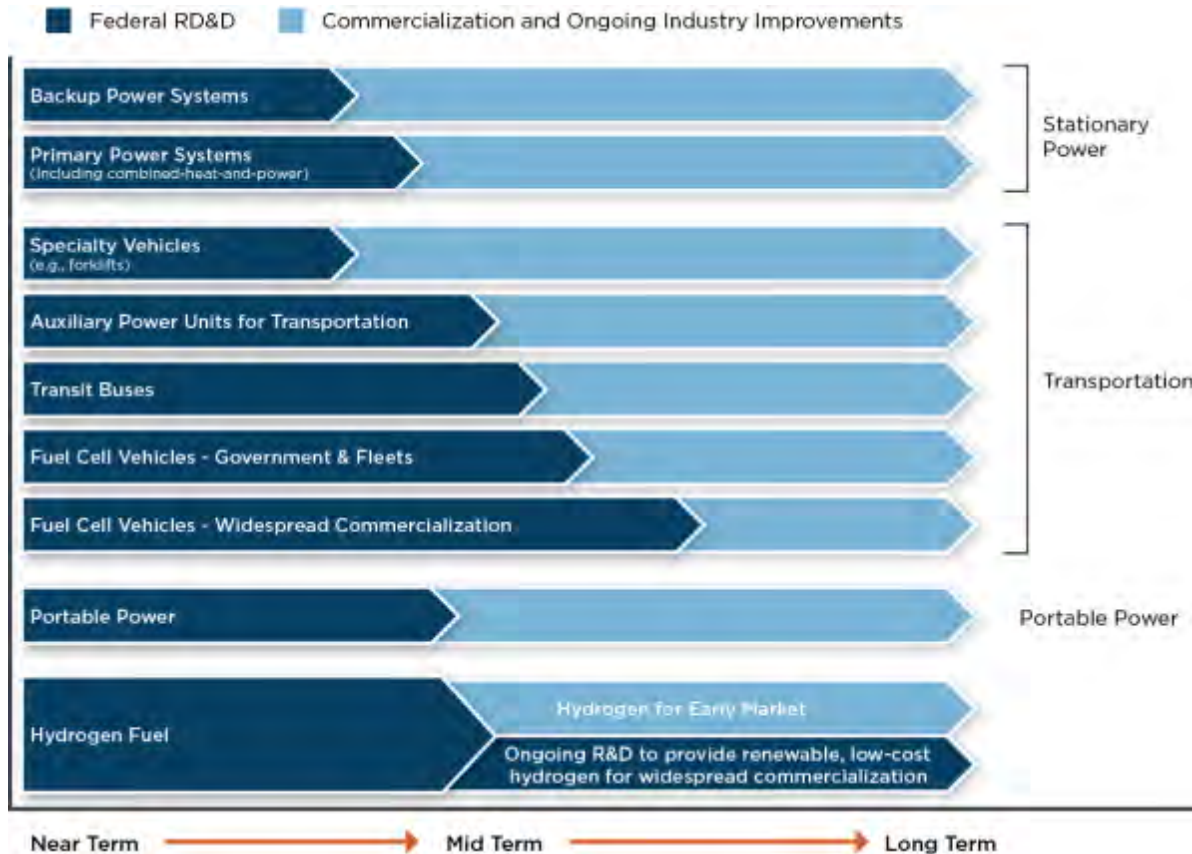
- up to 90% reduction in criteria pollutants for CHP systems

Fuel Flexibility

- **Clean fuels** — including biogas, methanol, H₂
- **Hydrogen** — can be produced cleanly using sunlight or biomass directly, or through electrolysis, using renewable electricity
- **Conventional fuels** — including natural gas, propane, diesel

DOE H₂ Fuel Cells Program Strategy

DOE's Hydrogen and Fuel Cells Program follows an integrated strategic plan for research, development, and demonstration activities

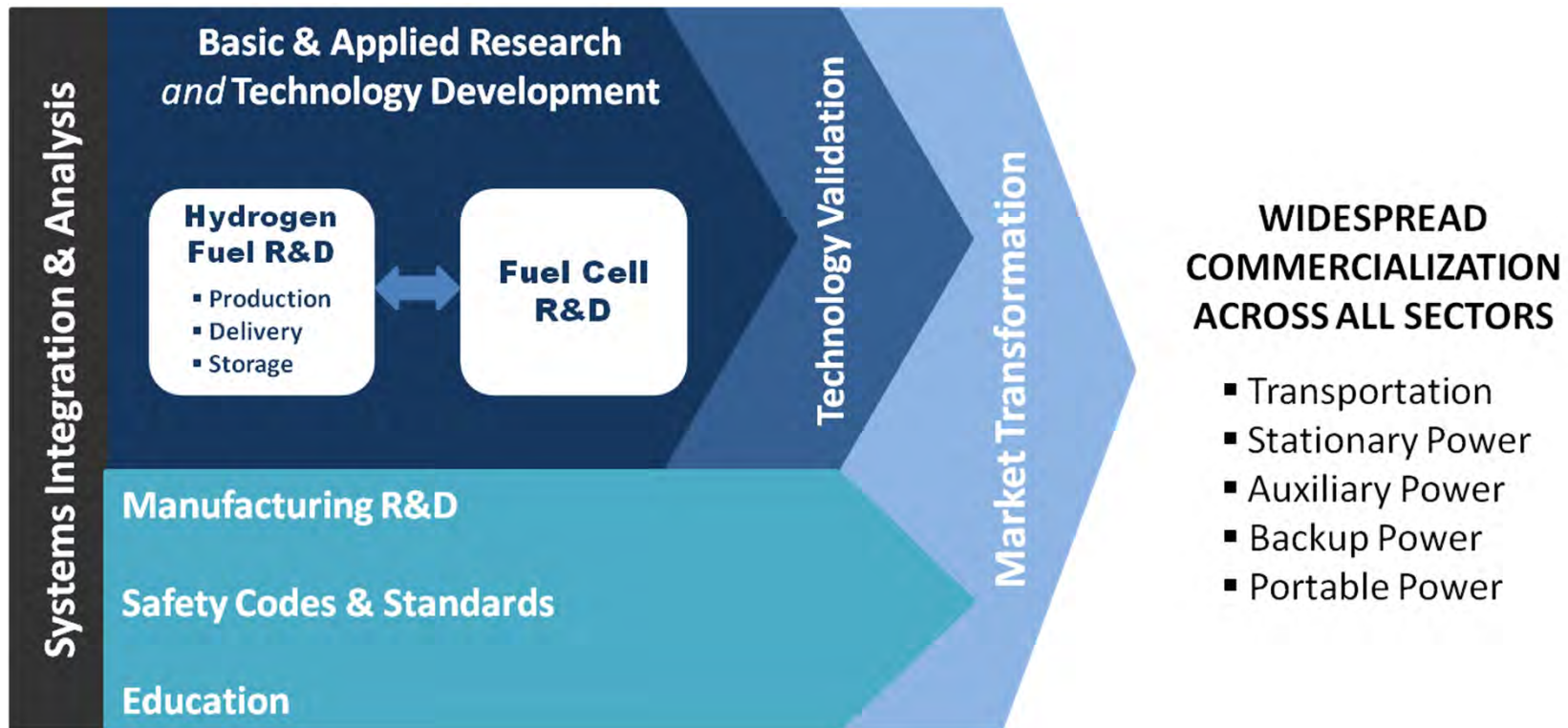


**Update to the
Hydrogen Posture
Plan (2006)**

Released September 2011

Program efforts are planned to transition to industry as technologies reach commercial-readiness.

http://www1.eere.energy.gov/hydrogenandfuelcells/pdfs/program_plan2011.pdf



*Nearly 300 projects currently funded
at companies, national labs, and universities/institutes
More than \$1B DOE funds spent from FY 2007 to FY 2011*

Targets are for complete systems, therefore engineering analysis is needed to project system characteristics/properties

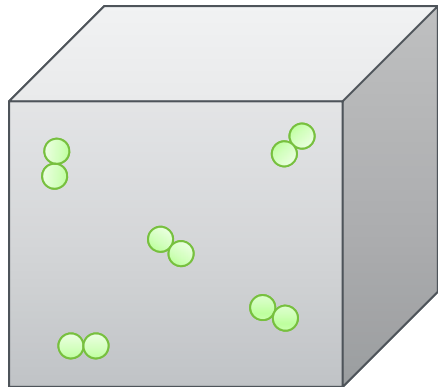
Storage Target	Units	2010	2017	Ultimate
System Gravimetric Capacity: [Usable net energy/H ₂]	kWh/kg (kg H ₂ /kg system)	1.5 (0.045)	1.8 (0.055)	2.5 (0.075)
System Volumetric Capacity: [Usable net energy/H ₂]	kWh/L (kg H ₂ /L system)	0.9 (0.028)	1.3 (0.040)	2.3 (0.070)
Storage System Cost: [initial targets (\$/kWh): 4 (2010), 2 (2015)]	\$/kWh net (\$/kg H ₂)	TBD (TBD)	TBD (TBD)	TBD (TBD)

Complete listing of the ***more than 20*** DOE performance targets for onboard hydrogen storage systems for light-duty vehicles can be found online at:
http://www1.eere.energy.gov/hydrogenandfuelcells/storage/pdfs/targets_onboard_hydro_storage.pdf

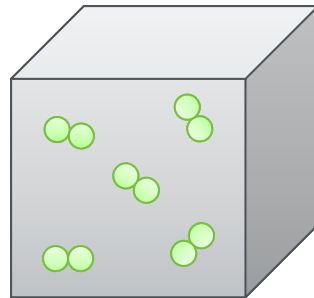
Challenge of Hydrogen Storage

Storing adequate amounts of hydrogen in an acceptably small volume in an efficient and cost-effective way is a critical challenge in commercialization of hydrogen technologies.

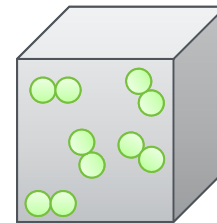
Physical Storage



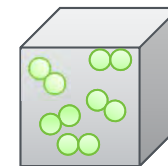
1 bar
normal
0.3 g/L



150 bar
lab cylinders
10 g/L



350 bar
Gen 1 vehicles
28 g/L

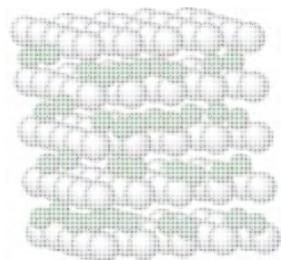


700 bar
Gen 2 vehicles
40g/L

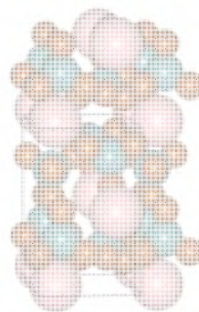


liquid H₂
71 g H₂/L
@ 20 K

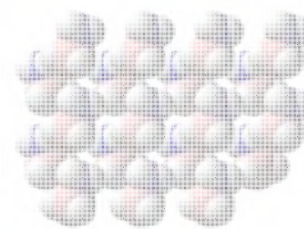
Materials-based Storage



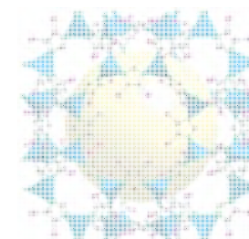
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~100-150 g H₂/L



complex hydrides
~70-150 g H₂/L

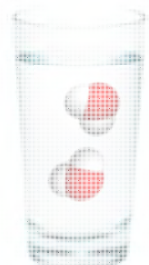


chemical storage
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sorbents
≤ 70 g H₂/L

Reference



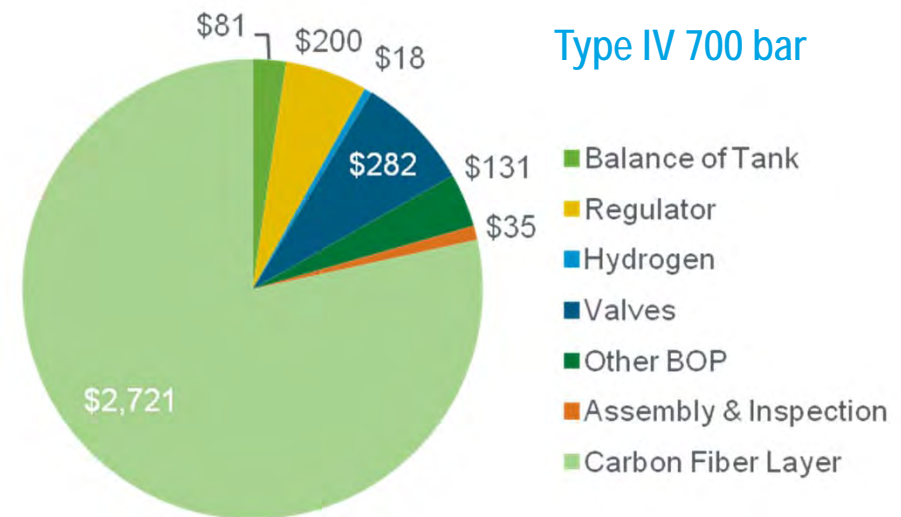
water
111 g H₂/L

Compressed gas storage offers a near-term option for initial vehicle commercialization and early markets.

Compressed gas storage offers a near-term option for initial vehicle commercialization and early markets

- Cost of composite tanks is challenging
- > 75% of the cost is projected to be due to the carbon fiber layer
- Additional analysis is needed to better understand costs at lower manufacturing volumes

Bulk of composite tank costs are in the carbon-fiber matrix



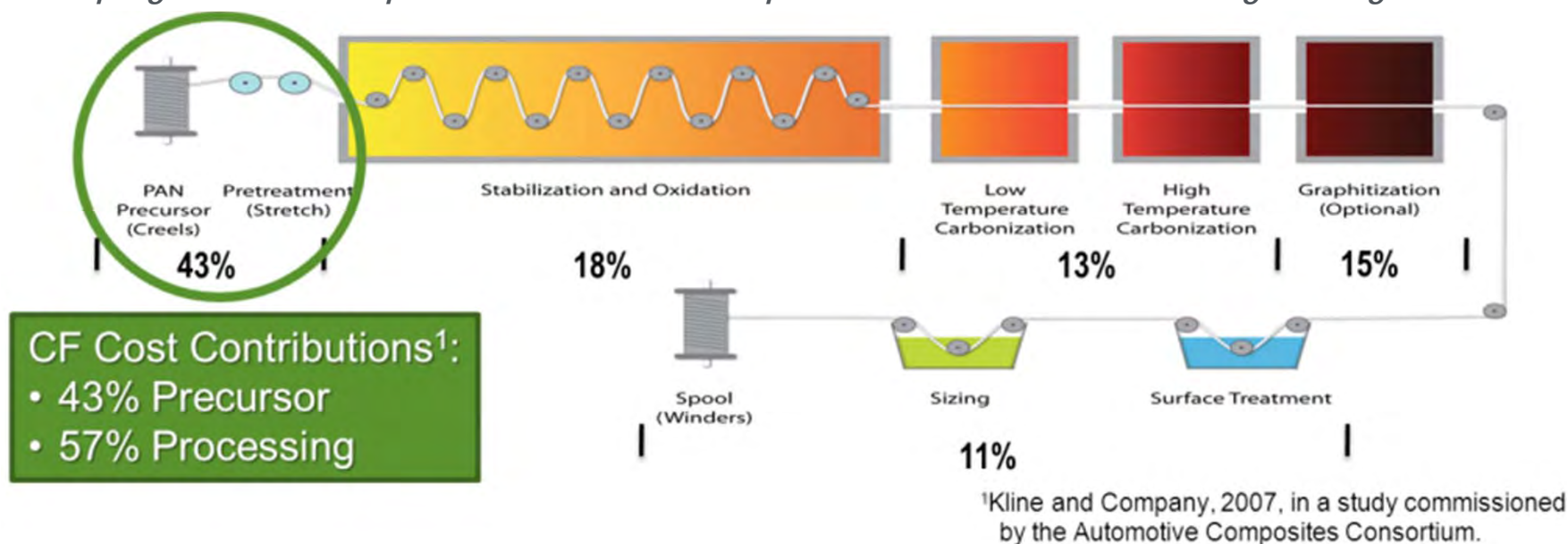
Tank Accomplishments

- Compressed H₂ tanks can achieve > 250 mile range
- Validated a vehicle that can achieve 430 mile range (with 700 bar Type IV tanks)

Carbon Fiber Cost is Key Focus Area

Understanding the costs associated with carbon fiber production is key to addressing barriers to lowering the costs of composite tanks.

Initiated programs to develop low-cost PAN fibers as precursors to reduce costs of high-strength carbon fibers



Objective: To produce low-cost PAN-based precursors for high strength CF²:

- Textile-grade PAN fibers with methyl acrylate comonomer – a 30-50% reduction in precursor costs
- Develop melt-spun PAN precursor technology - potential to reduce cost of the high strength CF's by ~ 30%.³

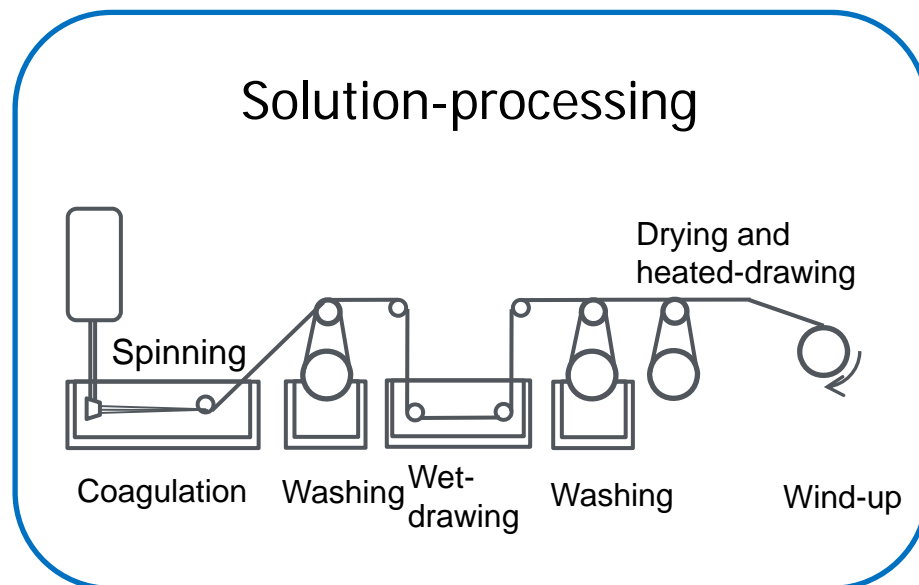
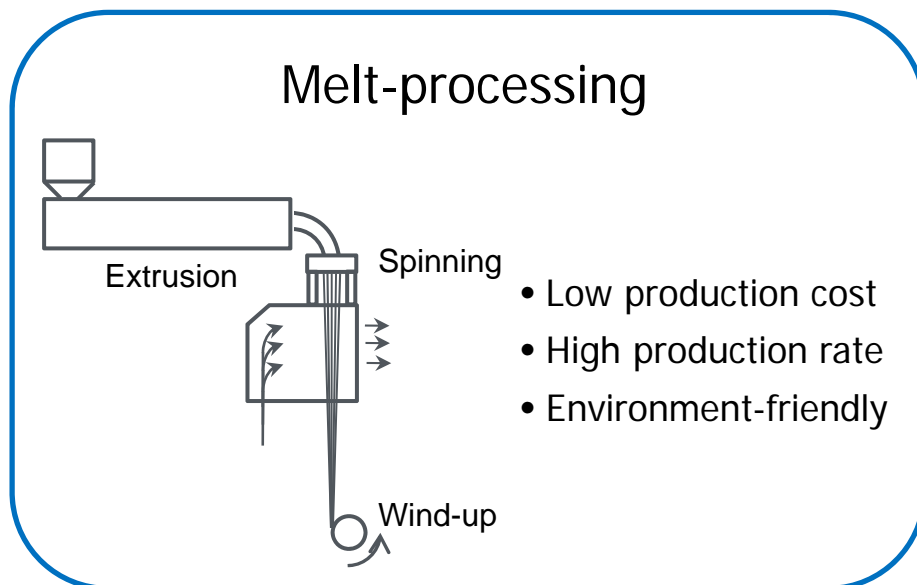
²PAN w/ MA precursor: ORNL with FISIPE; Melt-spun PAN precursors: ORNL w/ VT.

³[Kline & Company, 2007]

Carbon Fiber Cost is Key Focus Area

*Melt-spun PAN precursor technology has the potential to reduce the production cost of the high strength CF's by ~ 30%.**

Melt spin processing much less capital intensive than traditional wet spin technology



ORNL-Virginia Tech team has demonstrated melt spinnable PAN/MA with physical properties approaching commodity grade PAN

*: [Kline & Company, 2007]

Benefits vs Traditional Wet Spun Processing:

- ~ 30% lower precursor plant capital investment
- ~ 30% lower precursor plant operating cost
- Typical precursor line speed increased by $\geq 4X$ at winders

Cost Reduction Efforts:

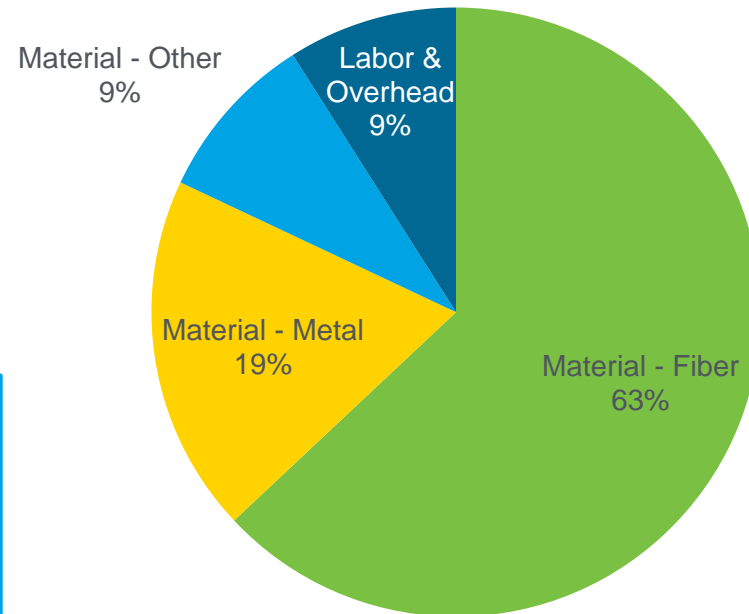
- Advanced manufacturing process combining filament winding with advanced fiber placement
- Hybrid tank design using lower cost carbon fiber on exterior layers
- Alternative fiber evaluation (Basalt)
- Manufacturing Process Automation

Accomplishments

Optimizing elements of advanced fiber placement & commercial filament winding led to a ~23% reduction in composite mass to 58.6 kg.

~25% strain decrease from outside to inside layers using lower cost fibers on exterior. Preliminary analysis shows a weight increase of 2.7% and a cost savings of 4%.

Tank Total Manufacturing Cost



Cost Breakdown Uses Following Assumptions:

125 liter 10,000 psi H₂ tank, Traditional manufacturing processes, Type IV (plastic liner) tank, Annual Production Quantity 10,000, Carbon fiber cost at \$15/lb, Metal components are 316L stainless steel

Manufacturing process automation includes automated resin mix system and winding station for increased facility throughput and reduction of product variation.

Composites for Hydrogen Tube Trailers

Use of composite vs. steel tubes increase trailer capacity from 400 kg to 600 kg and reduce capital cost to \$450/kg H₂ stored

Issue:

- Steel tube trailers weight limited
 - ▶ Capacities of up to 400 kg H₂ at ≤ 200 bar

Solution:

- Composite tube trailers volume limited
 - ▶ Capacities of up to 600 kg H₂ at 250 bar
 - ▶ A projected reduction in tube trailer delivery cost of > 33%

Further Improvements Possible:

- ▶ Vessel pressure can be increased an additional 100 bar (350 bar)
- ▶ increasing carrying capacity an additional 33% (800 kg H₂)
- ▶ reducing transport costs another 10%
- ▶ Identified a route to increase capacity to 1,100 kg H₂ and reduce trailer cost by 50% using cold compressed glass fiber vessels



Lincoln Composites and LLNL

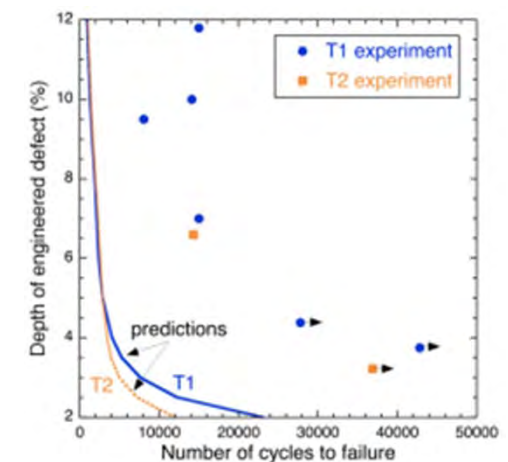
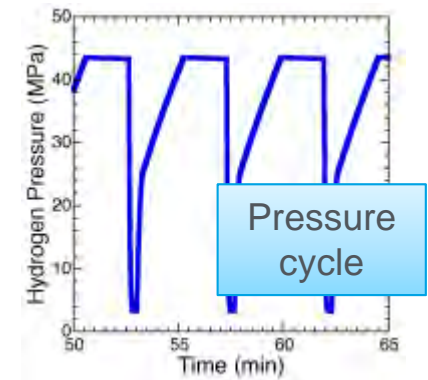
Addressing Performance and Safety: Tank Cycling

Full-scale pressure vessel testing supporting CSA HPIT1 standard development

Perform testing to simulate service in fuel-cell application

- Engineered defects used to evaluate defect tolerance
- Vessels cycled to failure or >30,000 cycles
- Cycle-life compared to ASME design calculations for hydrogen pressure vessels
- Materials testing in gaseous hydrogen also performed

- All observed failures were leak-before-break
- Cycle-life calculations (with engineered defects) are conservative by factor of 4 or more
- Results used to justify design requirements in CSA HPIT1 standard



Proposed design requirements

- Quench and tempered Cr-Mo steels
- S_u (ultimate strength) ≤ 890 MPa
- hoop stress $\leq 0.4 S_u$

Hydrogen Storage: Status for Compressed Gas

Targets are for complete systems, therefore engineering analysis is needed to project system characteristics/properties

Note: there are about 20 specific onboard storage targets that must be met simultaneously

Storage Targets	Gravimetric kWh/kg (kg H ₂ /kg system)	Volumetric kWh/L (kg H ₂ /L system)	Costs \$/kWh net (\$/kg H ₂)
2010	1.5 (0.045)	0.9 (0.028)	TBD (TBD)
2017	1.8 (0.055)	1.3 (0.040)	TBD (TBD)
Ultimate	2.5 (0.075)	2.3 (0.070)	TBD (TBD)

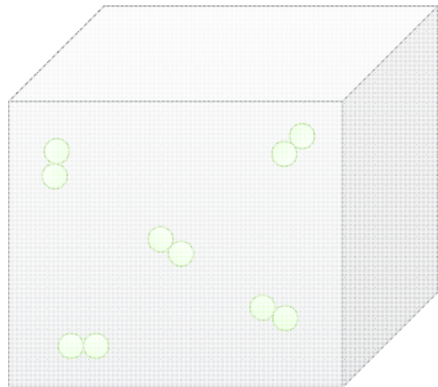
Current Status Notes - ^a : ANL/TIAX; ^b : HSECoE	Gravimetric	Volumetric	Costs
700 bar compressed (Type IV) ^a	1.7	0.9	18.9
350 bar compressed (Type IV) ^a	1.8	0.6	15.5
Cryo-compressed (276 bar) ^a	1.9	1.4	12.0*

*: Cost projections are from TIAX analyses of similar systems but not for the exact same design as the performance projections.

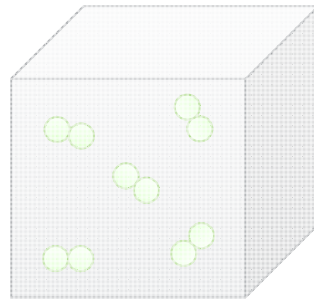
Challenge of Hydrogen Storage

Materials-based storage is considered to be a long-term solution to meet stringent volumetric targets and offer low-pressure storage solutions.

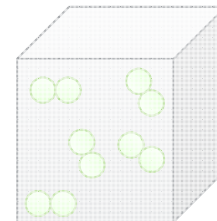
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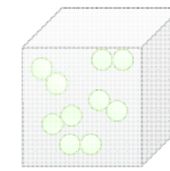
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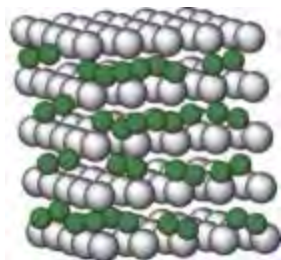


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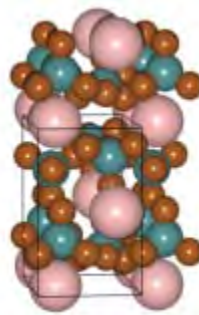


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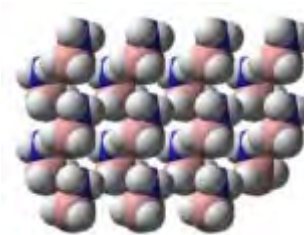
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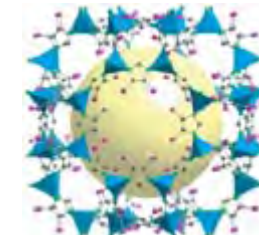
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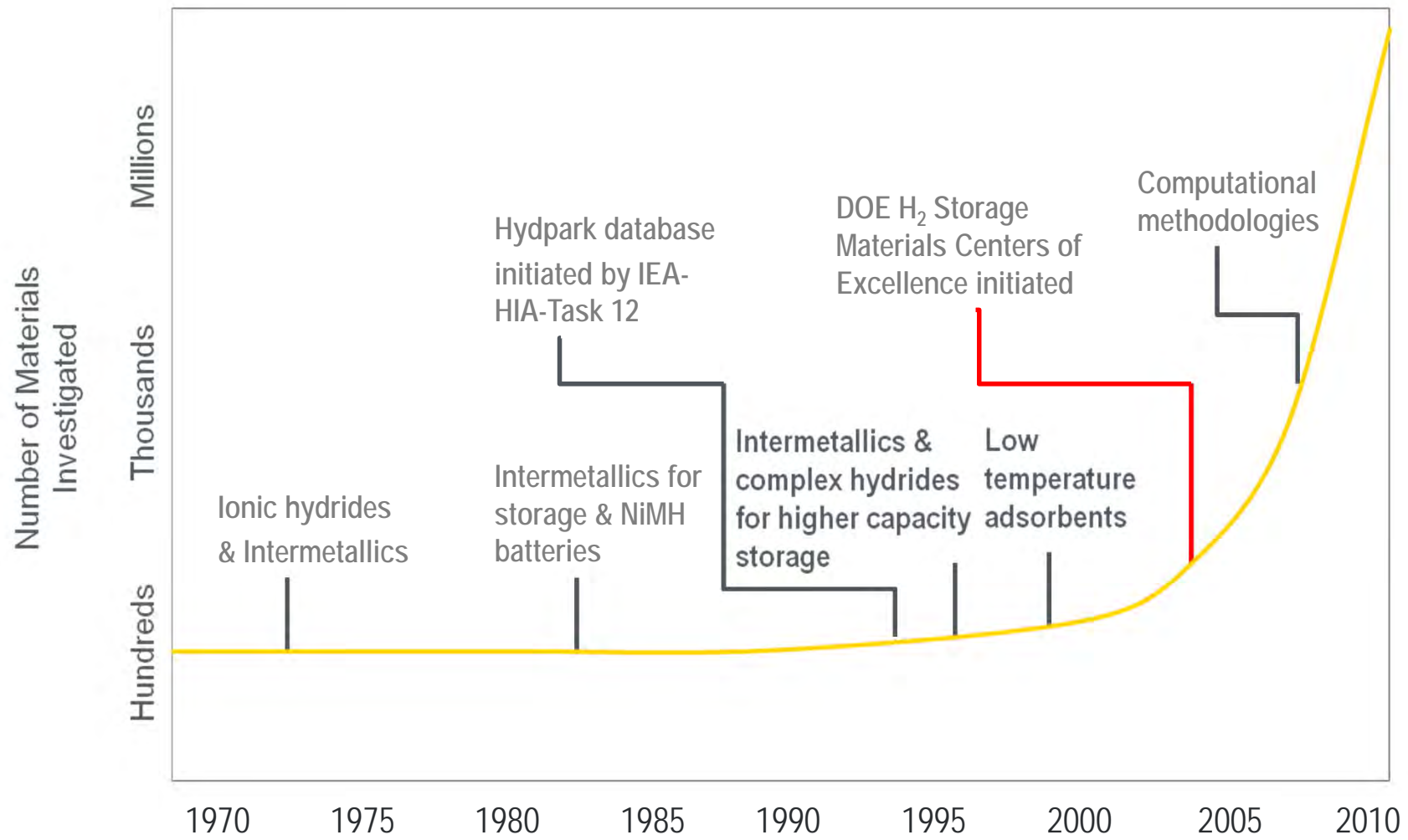
Reference



water
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Advancements in H₂ Storage Materials Research

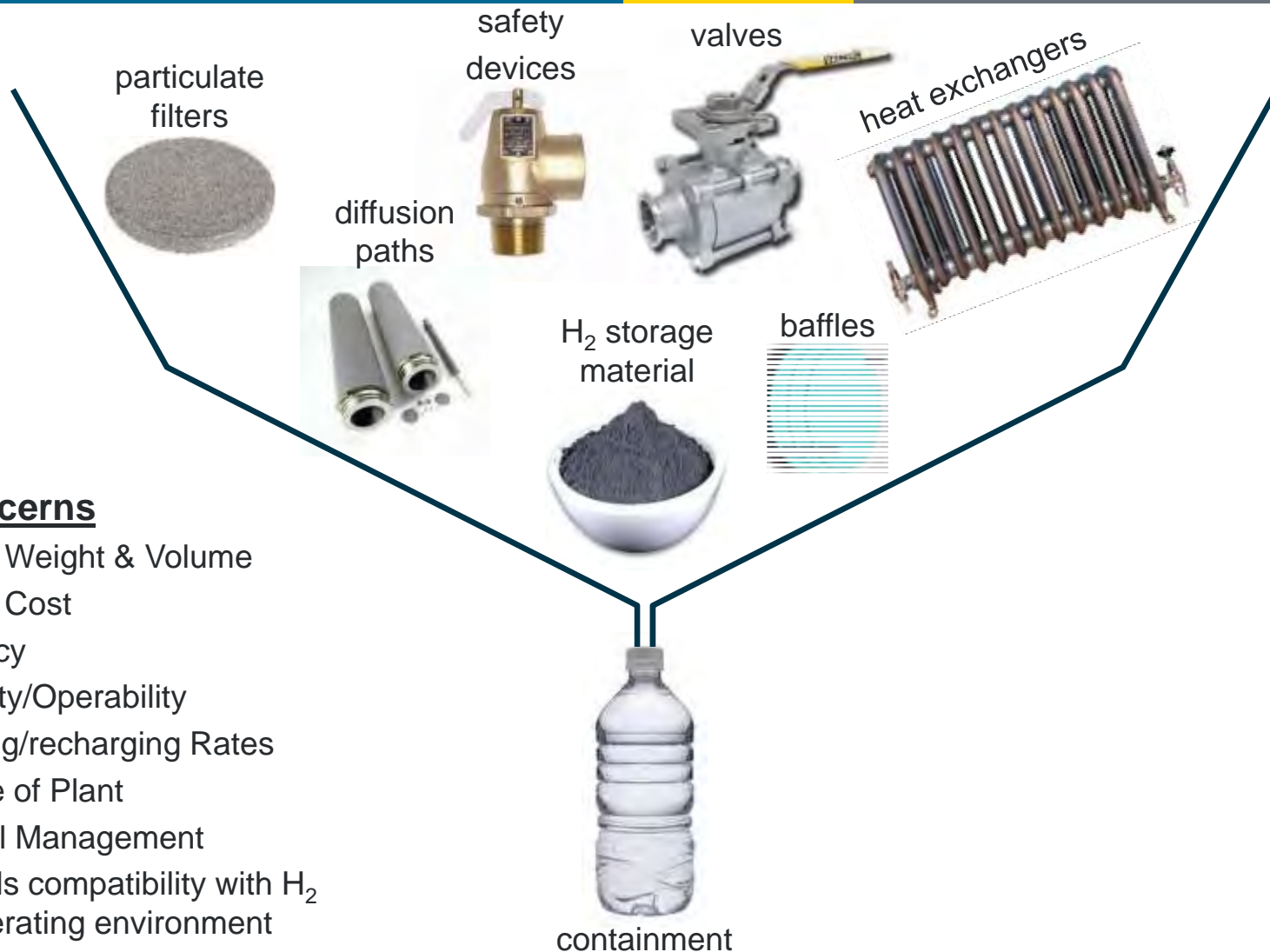
DOE Hydrogen Storage program's investments have led to exponential advances in the number of hydrogen storage materials studied by the end of 2010.



DOE Applied R&D investments on H₂ storage materials since 2001: >\$140M

Importance of System Engineering

System engineering is critical, enabling the development of complete integrated, low-cost hydrogen storage systems.

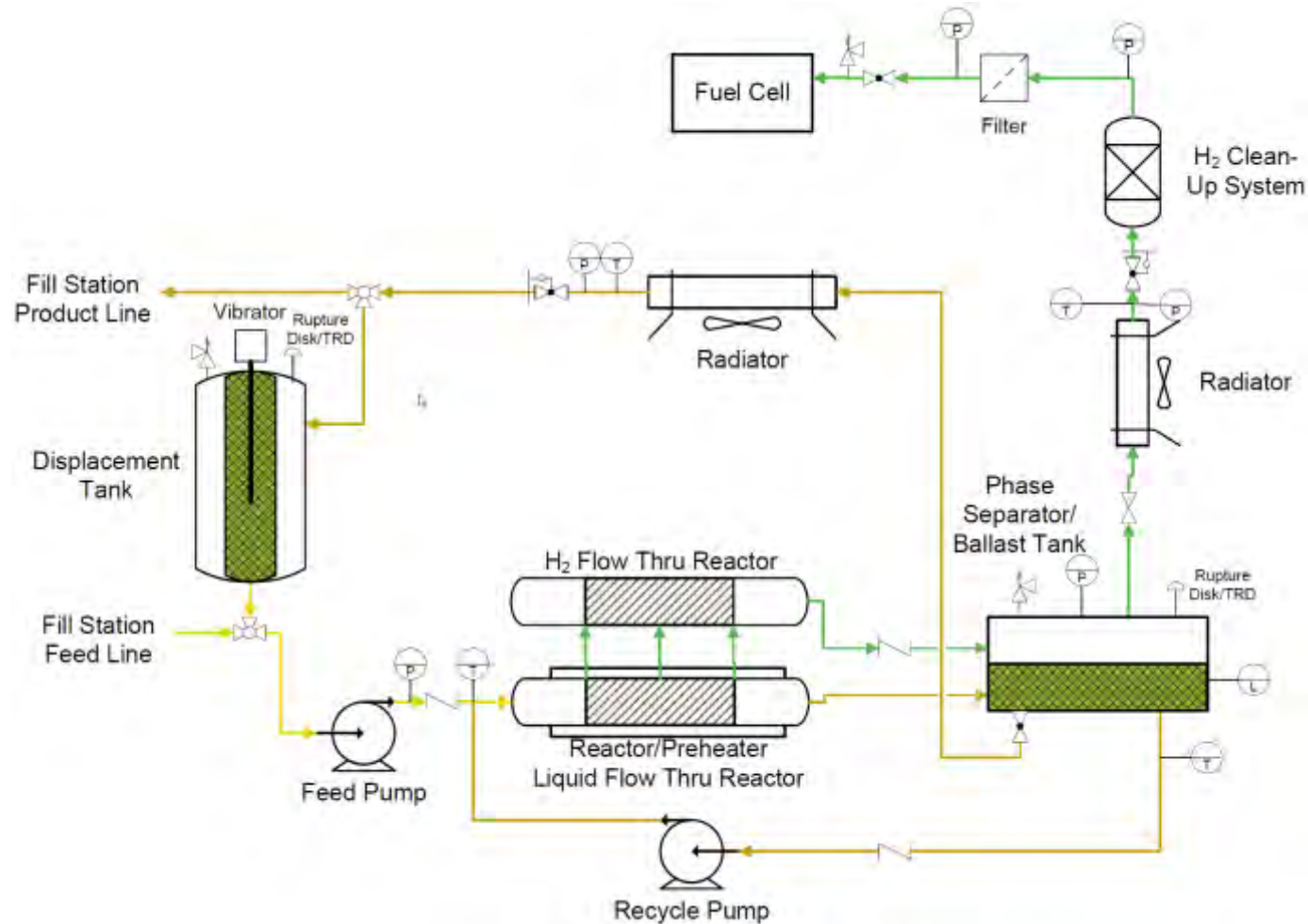


Key Concerns

- System Weight & Volume
- System Cost
- Efficiency
- Durability/Operability
- Charging/recharging Rates
- Balance of Plant
- Thermal Management
- Materials compatibility with H₂ and operating environment

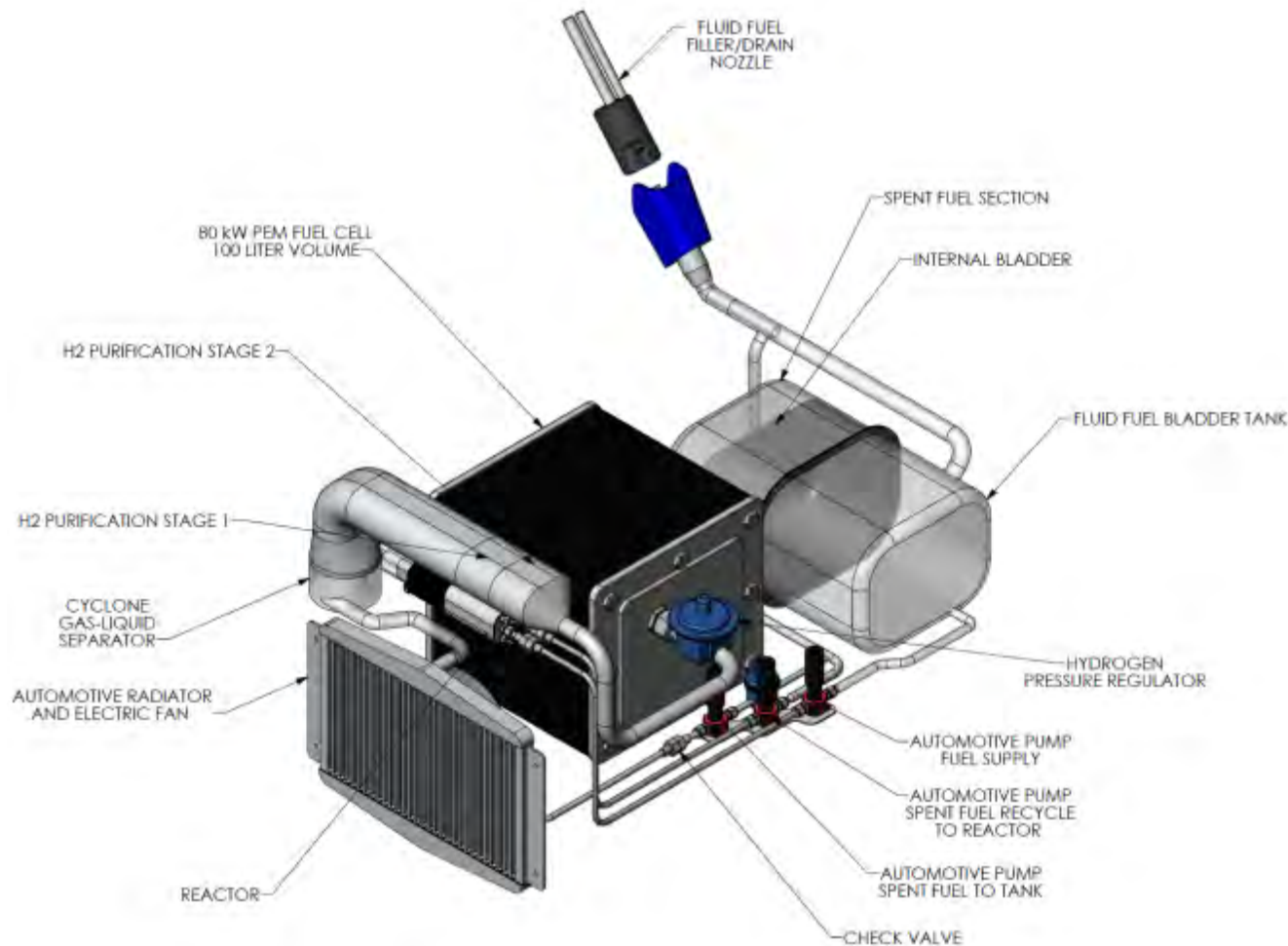
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The successful incorporation of all important elements in a practical package appropriate for the application is essential for a successful hydrogen storage system.

H₂ Storage Engineering Center of Excellence (HSCoE)

The HSECoE efforts helps to determine required material properties to guide materials development efforts for onboard vehicle storage applications.

- Developed complete, integrated systems models for 3 material classes
- Established baseline system performance with state-of-the-art design and best-of-class materials

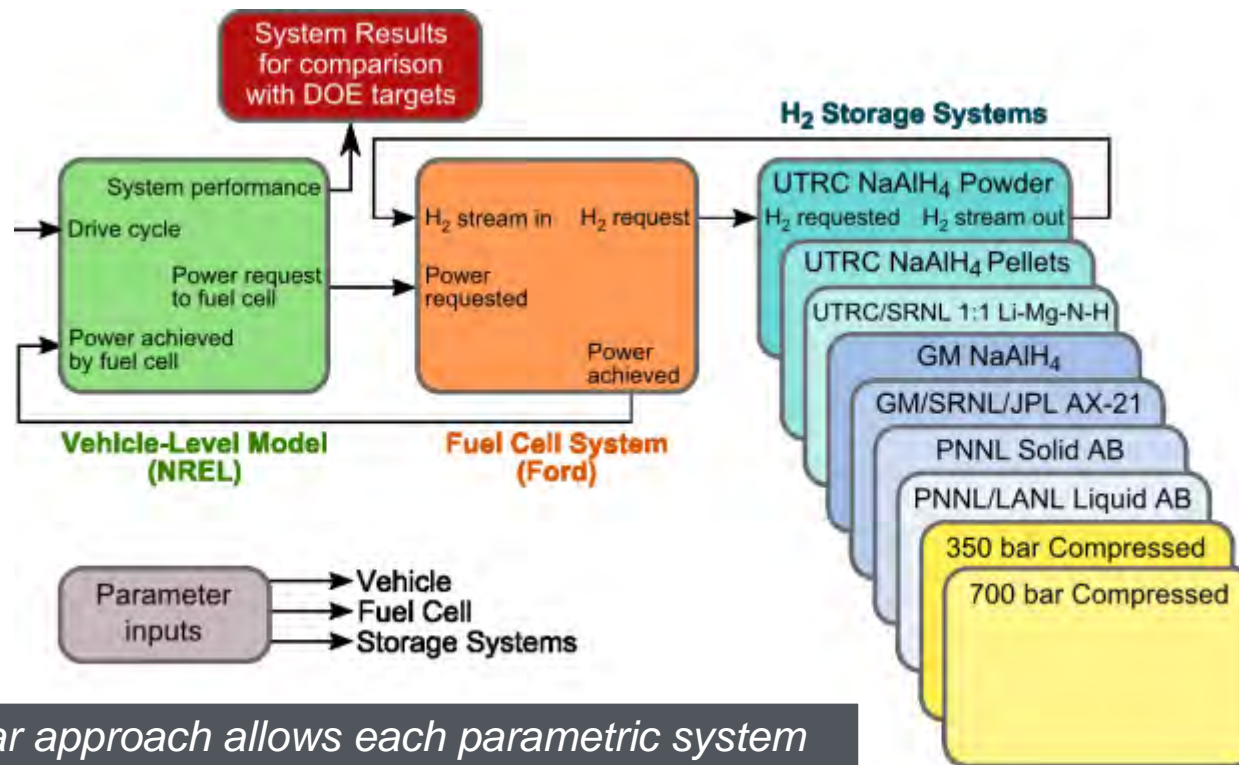
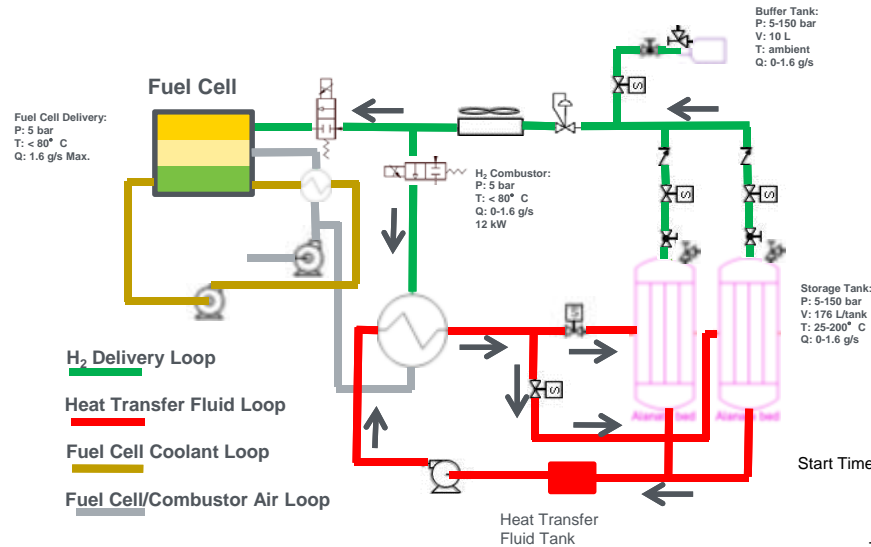


Figure courtesy of José Miguel Pasini, UTRC

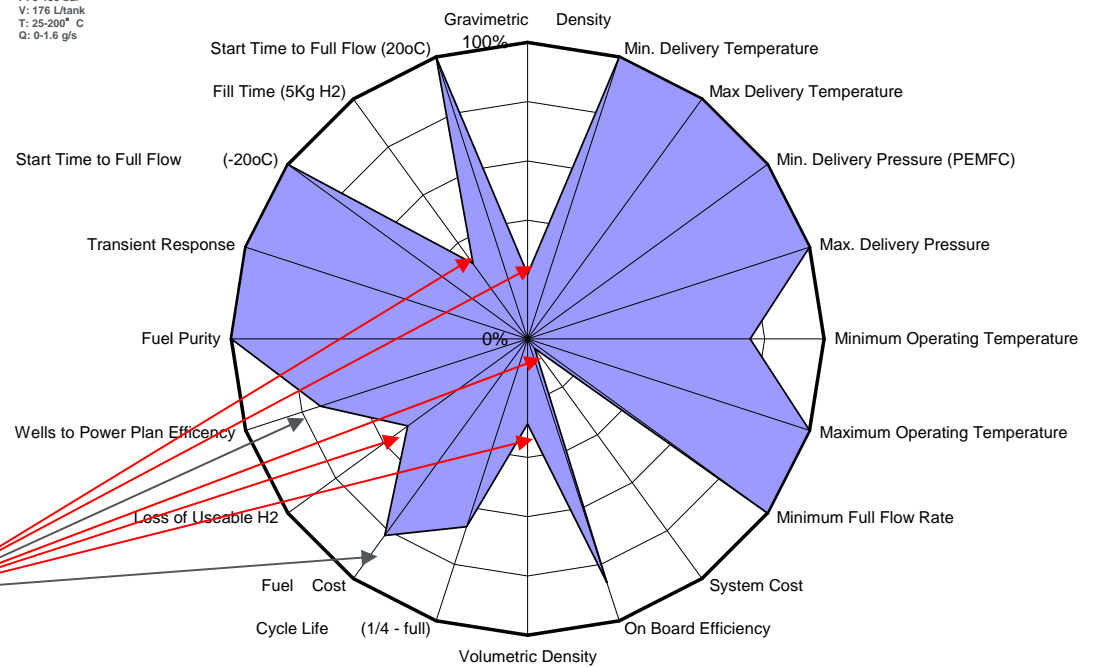
Modular approach allows each parametric system model be run through simulated drive cycles with fuel cell and vehicle-level models to predict performance.

Status of Metal Hydride Systems

No metal hydride material currently exists that will allow a complete system to meet all key DOE system performance targets for onboard vehicle applications



Results based on a dual tank, Sodium Alanate System

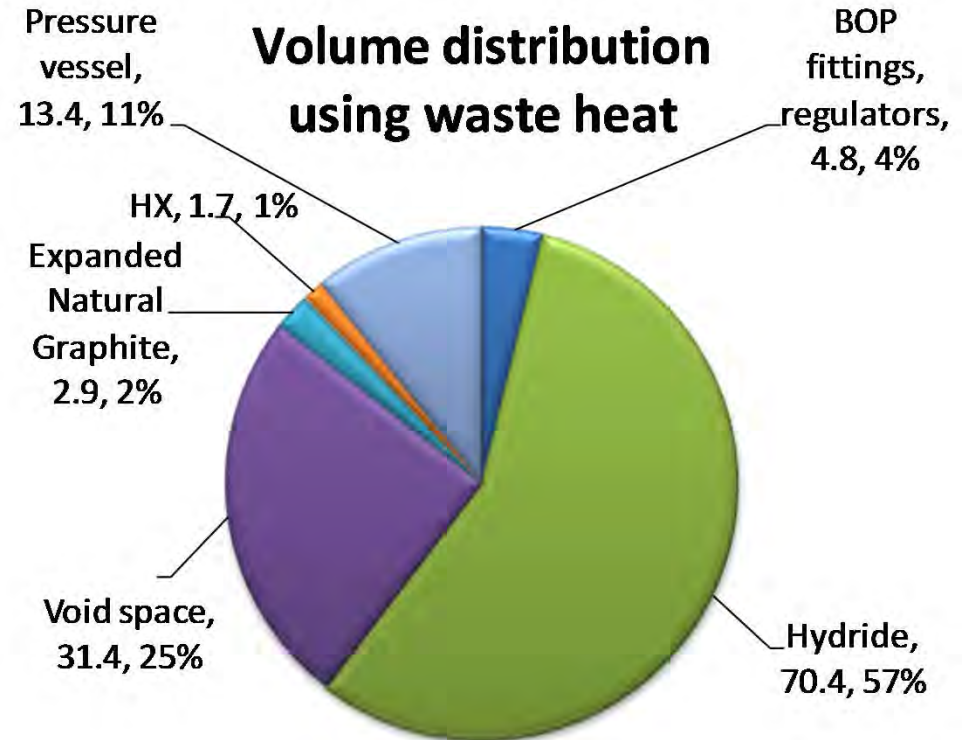
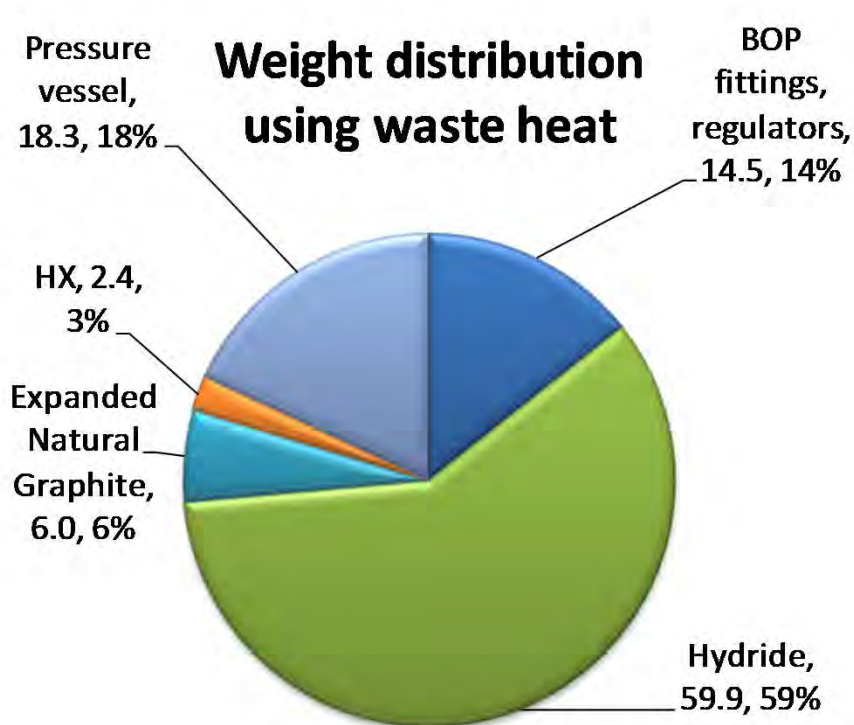


1. Gravimetric Density
2. System Cost
3. Onboard Efficiency
4. Volumetric Density
5. Fill Time
6. Fuel Cost
7. WPP Efficiency

Metal Hydride Requirements

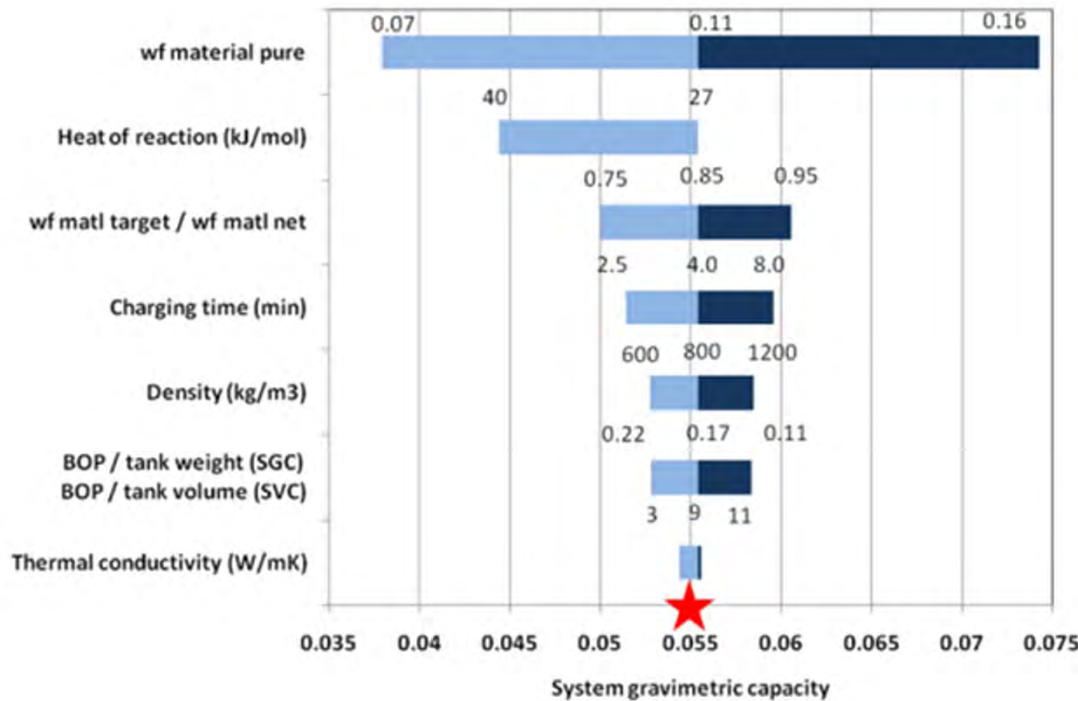
- Enthalpy such that waste heat use only

- Satisfies all DOE targets.
- $\Delta H = 27 \text{ kJ/mol-H}_2$
- **11 wt% pure material capacity**
- T (5 bar) = 20.7 C
- On-board efficiency: ~100%
- System: 101 kg, 124 liters

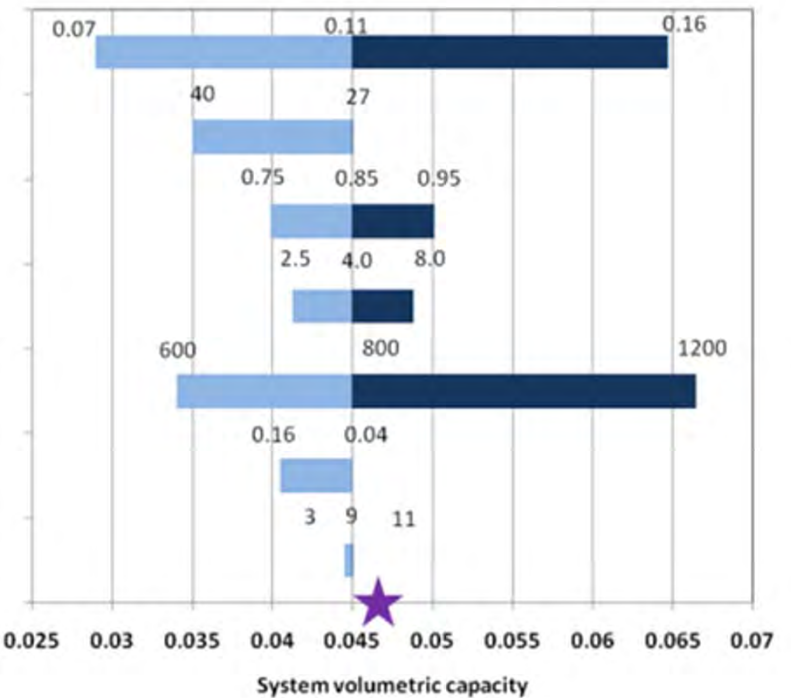


Sensitivity Analysis: System Gravimetric & Volumetric Capacity

System Gravimetric Capacity



System Volumetric Capacity

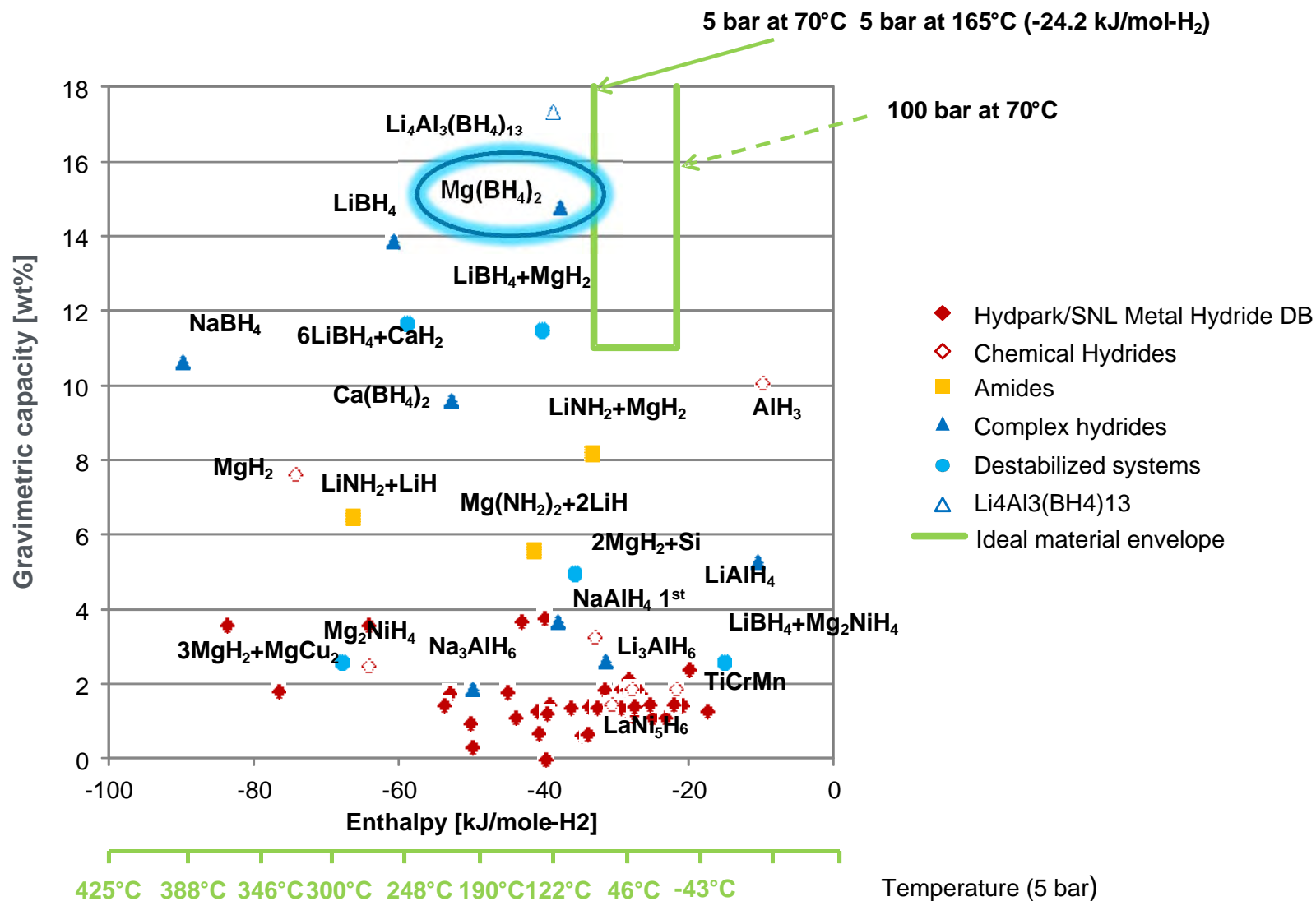


★ ★ DOE 2017 targets, gravimetric and volumetric capacity, respectively

Sensitivity Parameters (Baseline case)

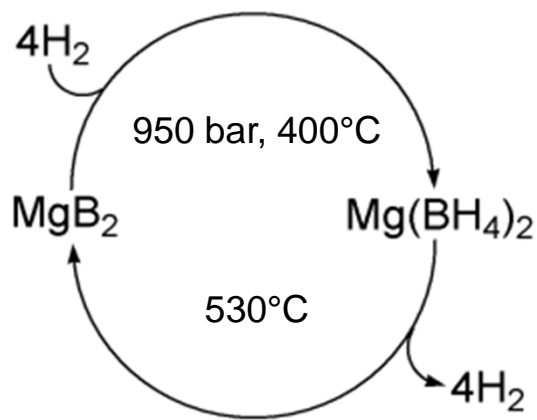
- Wf matl = 11%
- Heat of reaction = 27 kJ/molH₂
- Wf matl target / wf matl net = 85% *
- Charging time = 4 min
- Bulk density = 800 kg/m³
- BOP weight / tank weight = 17%
- BOP volume / tank volume = 4%
- Thermal conductivity = 9 W/mK *

Status: Gravimetric Capacity vs. Enthalpy

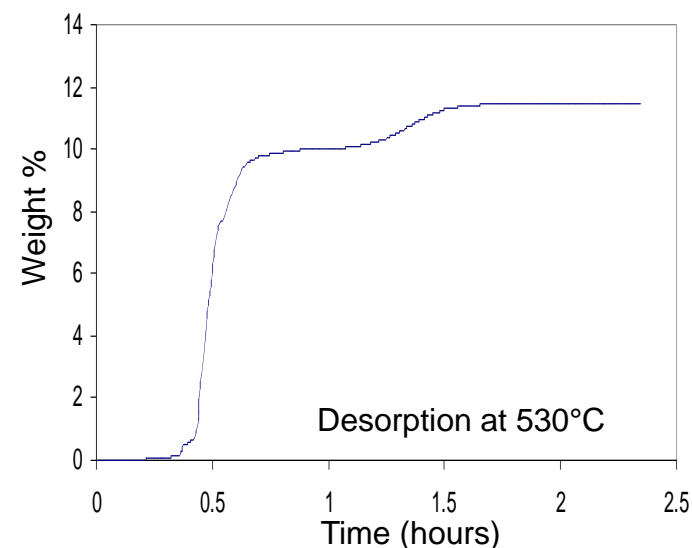


Recent Accomplishments for Metal Hydrides

12 wt.% reversible capacity demonstrated for $Mg(BH_4)_2$



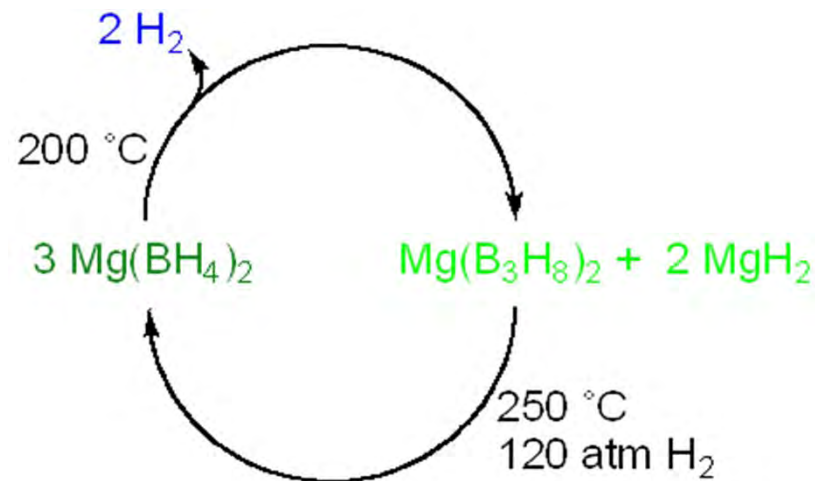
Evidence indicates that >14wt.% might be possible (theoretical capacity 14.8 wt.%)



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2.5 wt.% can be obtained under milder conditions by cycling between $Mg(BH_4)_2$ and magnesium triborane [$Mg(B_3H_8)_2$]



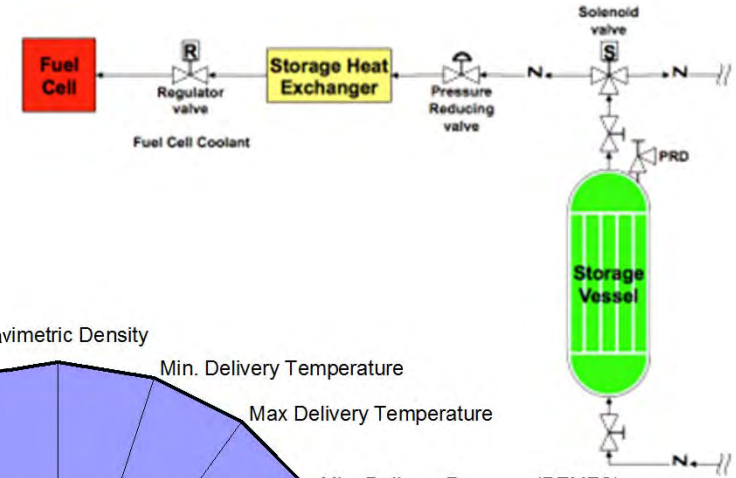
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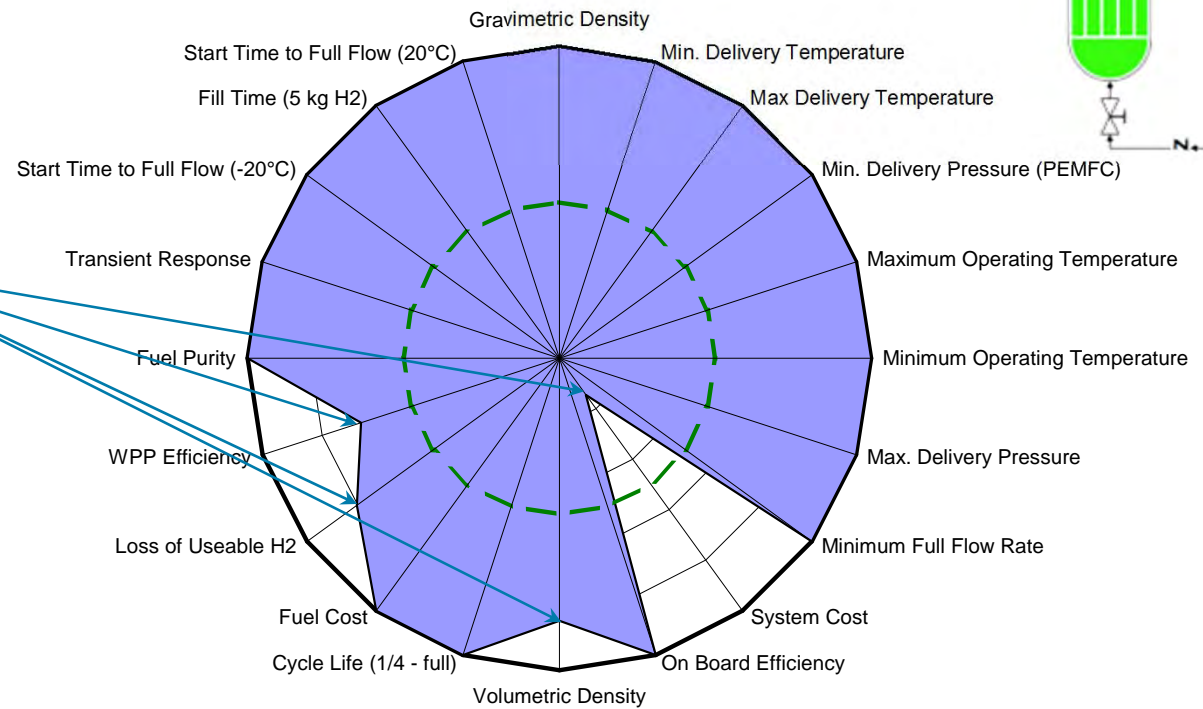
Status of Cryo-Sorbent Systems

Current cryo-sorbent system designs are projected to meet most DOE performance targets for onboard vehicle applications

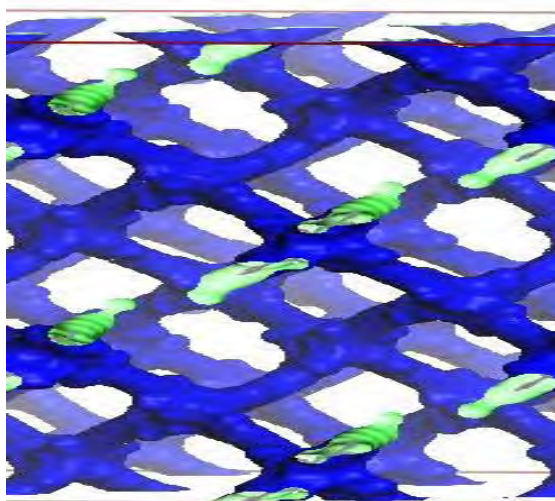
**Results based on a MOF-5 system,
200 bar, 80 K**



1. Volumetric Density
2. System Cost
3. Loss of Usable H₂
4. WPP Efficiency



*New sorbent materials synthesized with surface areas of $>6000 \text{ m}^2/\text{g}$
with material capacities over 8 wt% at 77K and $<100 \text{ bar}$*

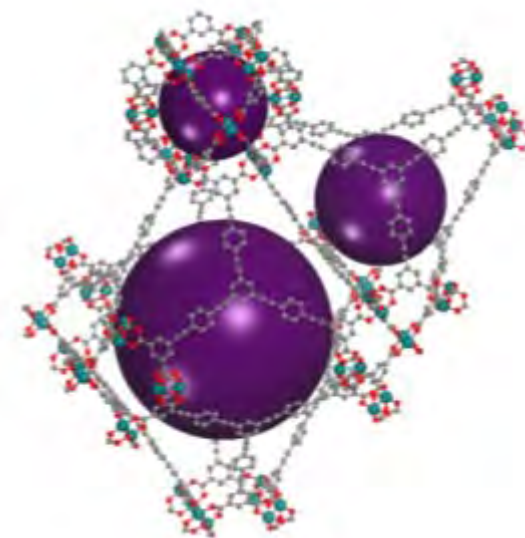


- Verified excess capacities greater than 8 wt.% at $\leq 70 \text{ bar}$ and 77 K
- BET surface areas exceeding $6000 \text{ m}^2/\text{g}$



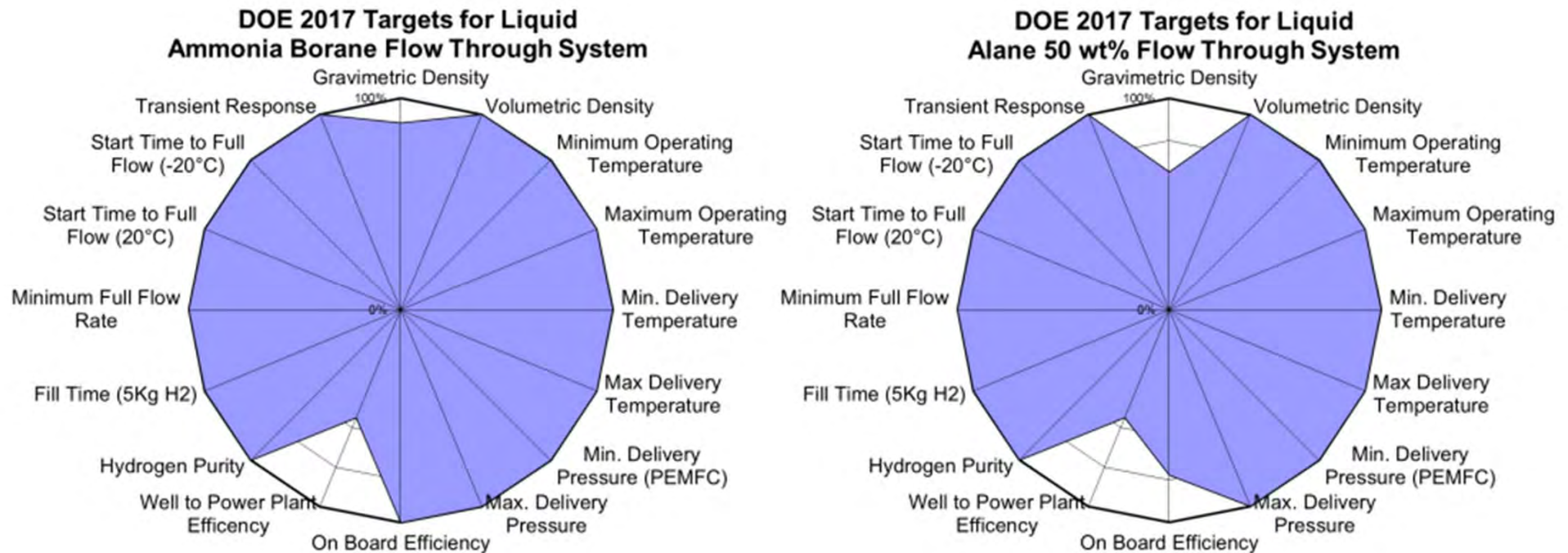
• Future efforts:

- need to increase isosteric heats of adsorption to increase sorption capacities at temperatures greater than cryogenic
- materials with higher hydrogen densities are needed



Endo- and Exothermic release material systems can meet most key DOE system performance targets for onboard vehicle applications

Projections for Exothermic (Ammonia Borane) and Endothermic (Alane) Hydrogen Release Systems – 50% mass loaded fluids

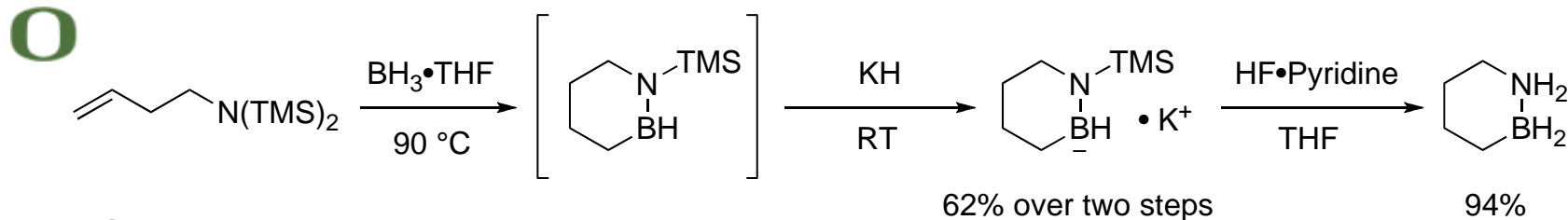


Off-board regeneration efficiency is still an issue

Recent Accomplishments in Chemical H₂ Storage Materials

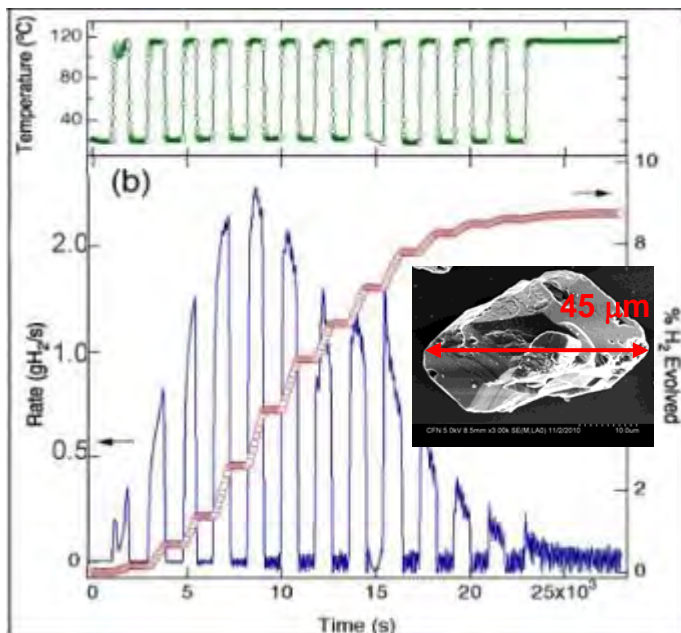
Catalysts and novel syntheses demonstrate improvements in kinetics and thermal control

Parent CBN synthesized that is air and thermally stable and delivers up to 1.5 equiv. H₂

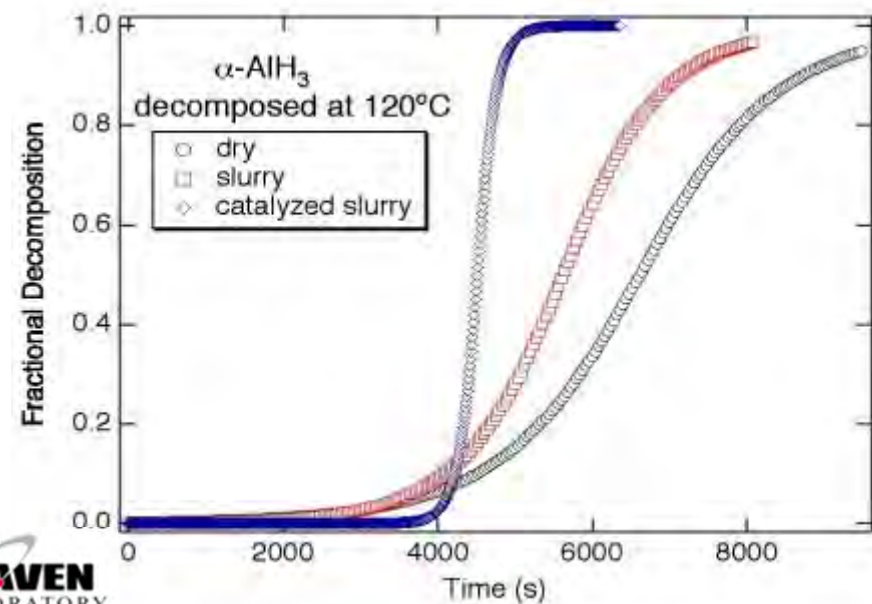


Synthesis of larger AlH₃ particles allows thermal control of decomposition

Ti Catalyzed 60 wt.% AlH₃ slurry demonstrates 2x faster H₂ than dry powder



BROOKHAVEN
NATIONAL LABORATORY



Status for Materials-based Hydrogen Storage Systems

Targets are for complete systems, therefore engineering analysis is needed to project system characteristics/properties

Note: there are about 20 specific onboard storage targets that must be met simultaneously

Storage Targets	Gravimetric kWh/kg (kg H ₂ /kg system)	Volumetric kWh/L (kg H ₂ /L system)	Costs \$/kWh net (\$/kg H ₂)
2010	1.5 (0.045)	0.9 (0.028)	TBD (TBD)
2017	1.8 (0.055)	1.3 (0.040)	TBD (TBD)
Ultimate	2.5 (0.075)	2.3 (0.070)	TBD (TBD)

Current Status Notes - ^a : ANL/TIAX; ^b : HSECoE	Gravimetric (kWh/kg sys)	Volumetric (kWh/L sys)	Costs (\$/kWh)
Metal Hydride (NaAlH ₄) ^b	0.4	0.4	11.3*
Sorbent (MOF-5, 200 bar) ^b	1.7	0.9	18.0*
Off-board regenerable (AB) ^b	1.4	1.3	NA

*: Cost projections are from TIAX analyses of similar systems but not for the exact same design as the performance projections.

Projected reduction in installed pipeline costs of 15%



U. Illinois, SECAT, SNL, ORNL, SRNL

Issue:

- Capital costs are driven by joining and installation costs for current pipelines

Solution:

- Fiber reinforced polymer (FRP) pipelines
- Longer sections between joints and lower installation costs
- Demonstrated a 3x design margin for FRP through flaw tolerance testing
- Projected reduction in installed pipeline cost of 15%

Future Work

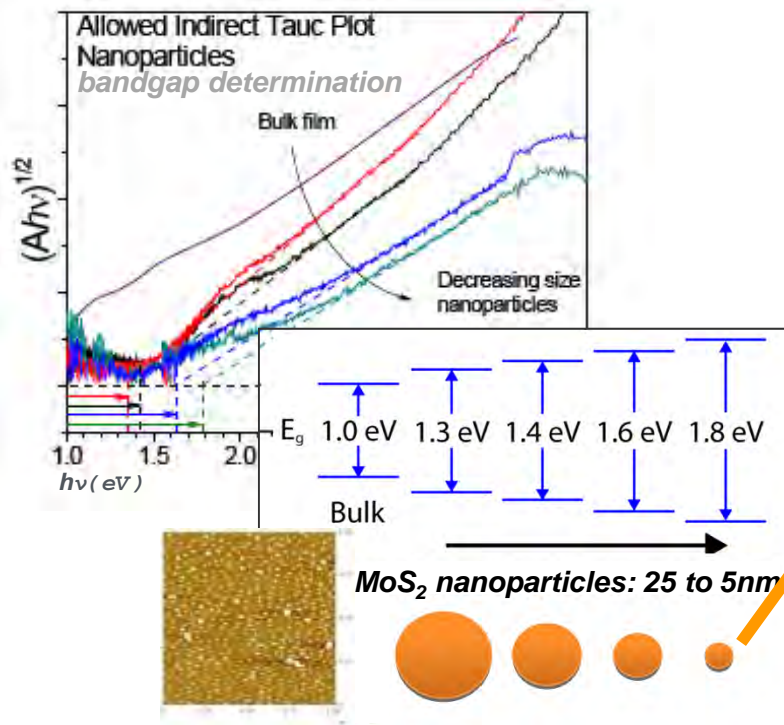
- Determined that the level of H₂ permeation through materials will meet DOE targets and FRP burst strength
- Demonstrated no degradation in FRP after 8mo of accelerated aging (equivalent to 5yrs at room temperature)

Nano-Catalyst System for Solar Hydrogen Production

Discovering new MoS₂ nano-catalysts, and developing novel macro-structures for integration into practical photoelectrochemical (PEC) hydrogen production devices

Fundamental Science:

Based on fundamental principles of quantum confinement, nanoparticle MoS₂ catalysts exhibit bandgap enlargement from 1.2 eV (bulk) to ~1.8 eV when diameter is reduced to ~5 nm.

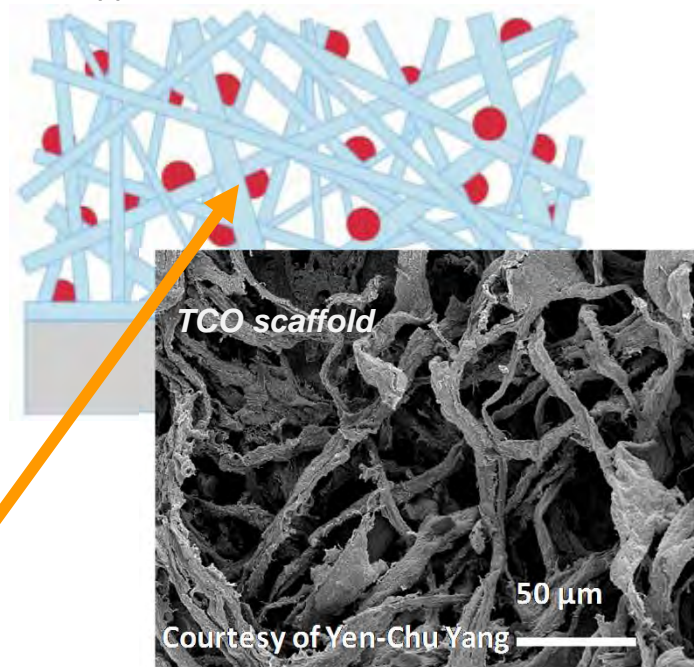


Bandgap blueshift in 5 nm MoS₂ nanoparticles sensitizes catalyst to efficiently absorb light in the solar spectrum

Source: T. Jaramillo, et al. *Science* 2007, 317, 100122; Y. Aoki, J. Huang, T. Kunitake, *J. Mater. Chem.*, 2006, 16, 292-297

Applied R&D:

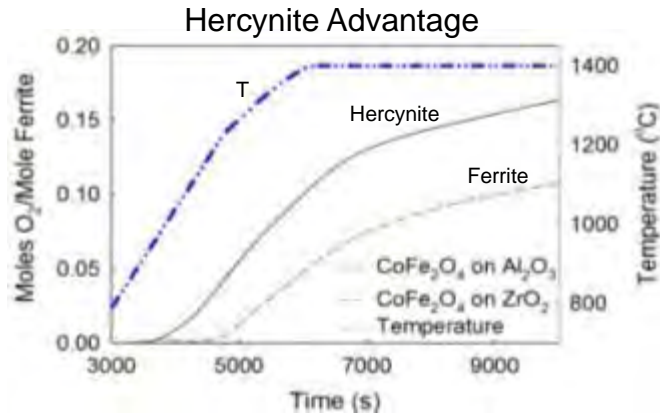
A macroporous scaffold consisting of a transparent conducting oxide (TCO) is being developed upon which the MoS₂ nanoparticles can be vertically integrated for support, confinement and electronic contact.



Scaffold is enabling technology for development of MoS₂ photoelectrodes for effective solar H₂ production

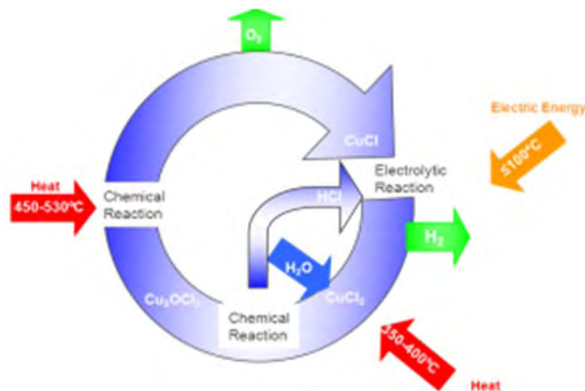
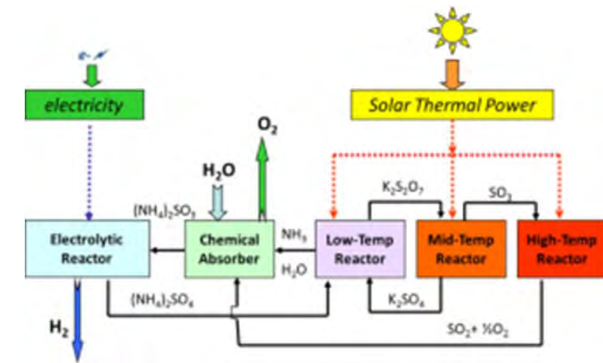


Advanced Materials: Key to Progress in STCH Production



Using ALD Ferrite, increased thin film peak production rate ~100x faster than bulk. Hercynite route shows advantages in reduced reduction temperature and larger operating window. (U of Colorado)

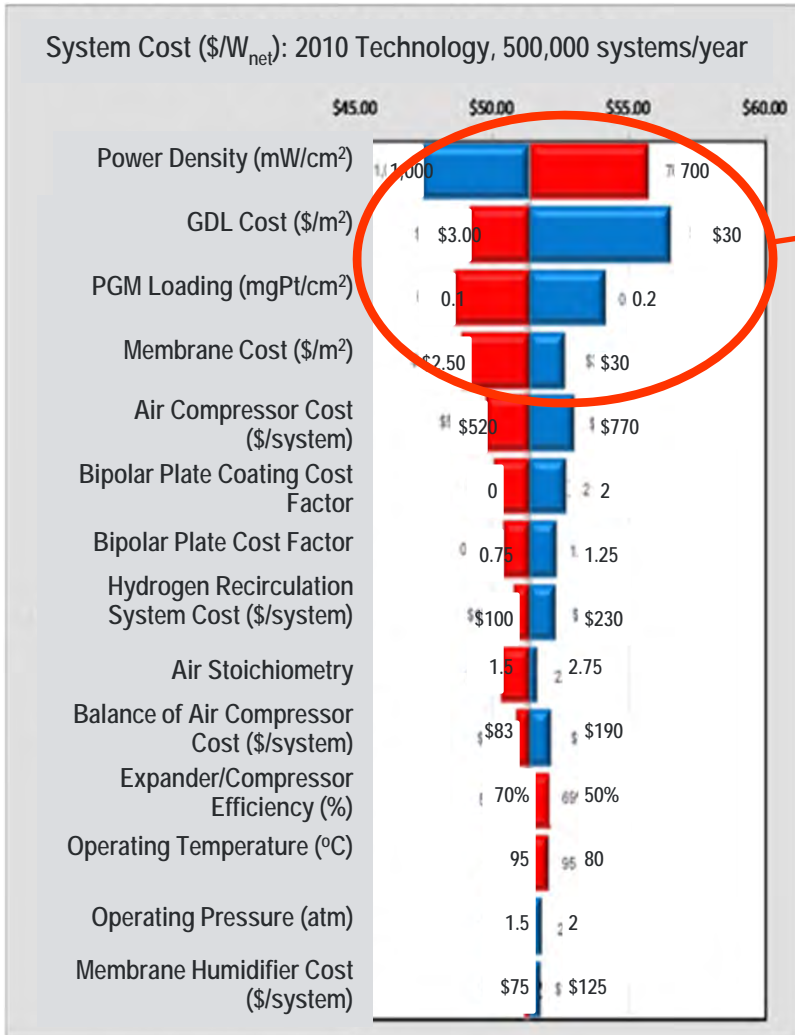
Down select of electrode and catalyst materials for high T, P testing. Voltage of the electrolytic cell has been reduced to values at 80°C, close to those previously obtained at 130°C. (SAIC)



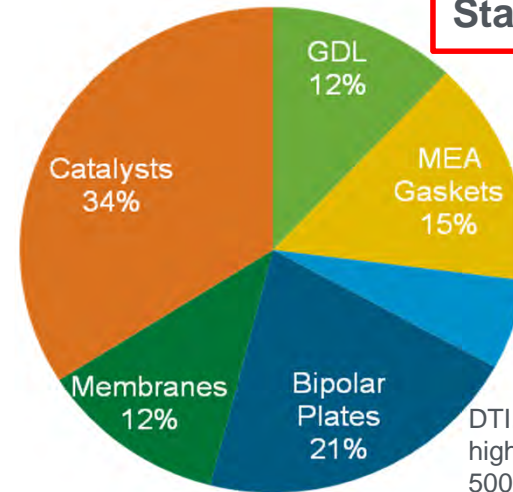
Two best membranes identified for Cu-Cl cycle with Cu diffusivity <10% of Nafion that are chemically and thermally stable at 80 C for over 40 hours. (ANL)

Fuel Cell Stacks – Costs and Durability

Challenges: Cost and Durability—must be met simultaneously
Platinum cost is ~34% of total stack cost. Catalyst durability needs improvement



Key Focus Areas for R&D



Stack Cost - \$25/kW

DTI, **2010 analysis**, scaled to high volume production of 500,000 units/yr. Used \$1100/Troy Ounce for Pt Cost

- ### Strategies to Address Challenges—Examples
- **Lower PGM Content:** Improved Pt catalyst utilization and durability
 - **Pt Alloys:** Pt-based alloys with comparable performance to Pt and cost less
 - **Novel Support Structures:** Non-carbon supports and alternative carbon structures
 - **Non-PGM catalysts:** Non-precious metal catalysts with improved performance and durability

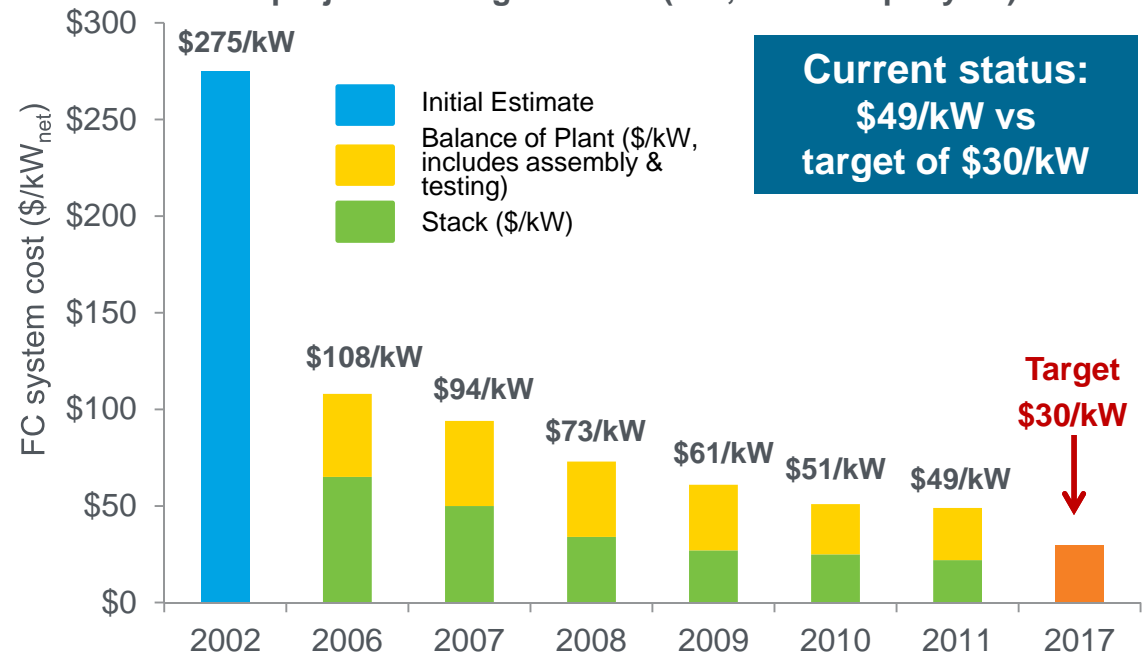
Programmatic Progress – Fuel Cells

Projected high-volume cost of fuel cells has been reduced to \$49/kW (2011)*

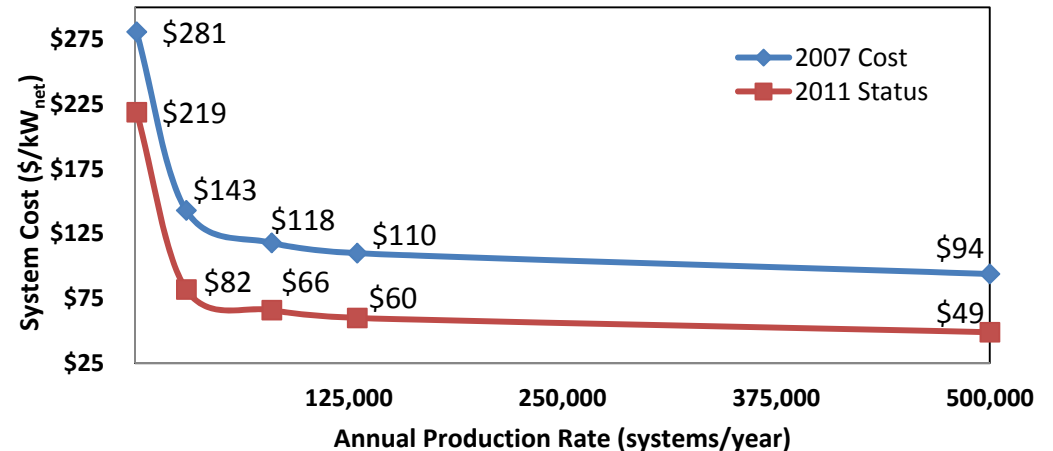
• **More than 30% reduction since 2008**

• **More than 80% reduction since 2002**

Projected Transportation Fuel Cell System Cost
-projected to high-volume (500,000 units per year)-



Projected Costs at Different Manufacturing Rates






*Based on projection to high-volume manufacturing (500,000 units/year). The projected cost status is based on an analysis of state-of-the-art components that have been developed and demonstrated through the DOE Program at the laboratory scale. Additional efforts would be needed for integration of components into a complete automotive system that meets durability requirements in real-world conditions.

Programmatic Progress – H₂ Production & Delivery



The revised hydrogen threshold cost is a key driver in the assessment of Hydrogen Production and Delivery R&D priorities.

Projected High-Volume Cost of Hydrogen Production¹ (Delivered²)—Status

Distributed Production (near term)

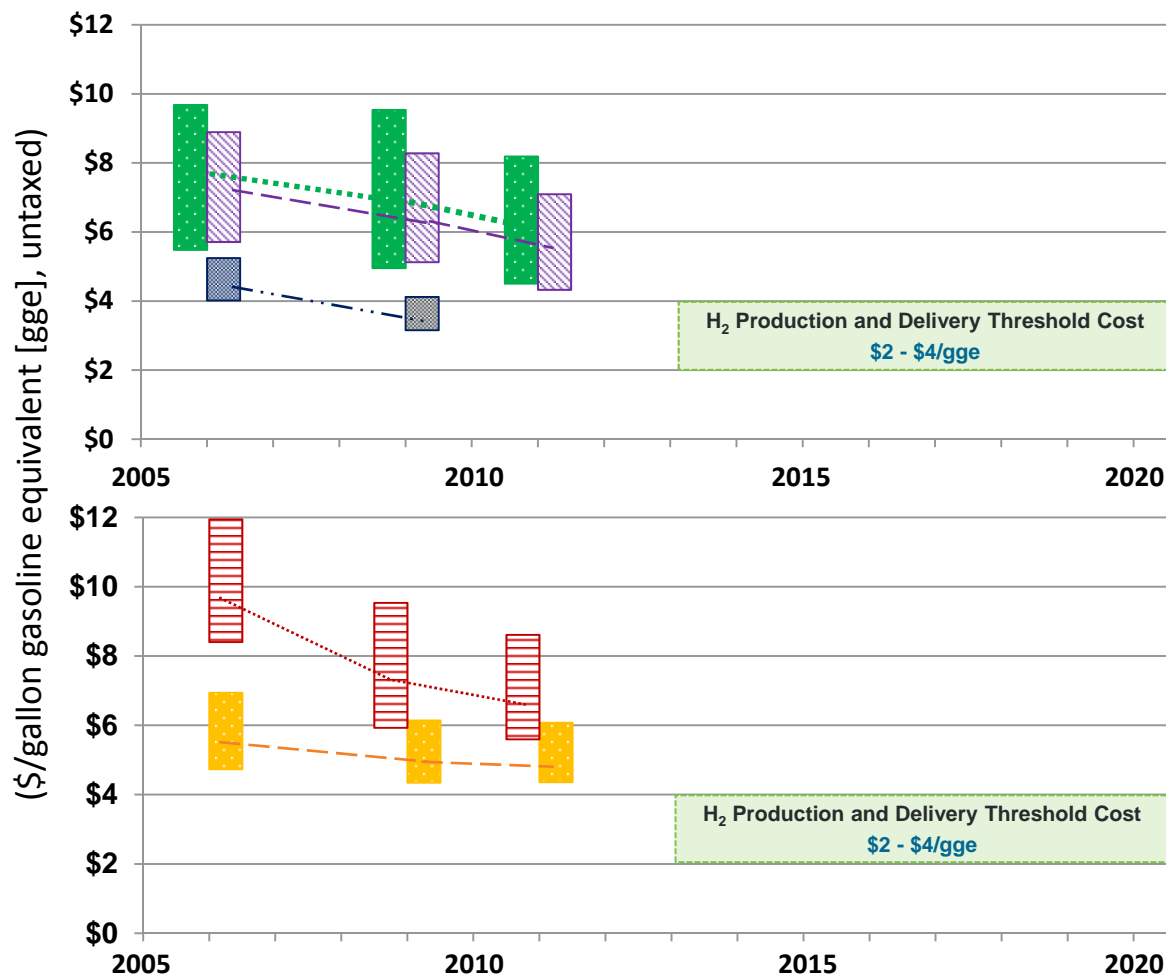
-  **Electrolysis**
Feedstock variability: \$0.03 - \$0.08 per kWh
-  **Bio-Derived Liquids**
Feedstock variability: \$1.00 - \$3.00 per gallon ethanol
-  **Natural Gas Reforming³**
Feedstock variability: \$4.00 - \$10.00 per MMBtu

Central Production (longer term)

-  **Electrolysis**
Feedstock variability: \$0.03 - \$0.08 per kWh
-  **Biomass Gasification**
Feedstock variability: \$40- \$120 per dry short ton

Notes:

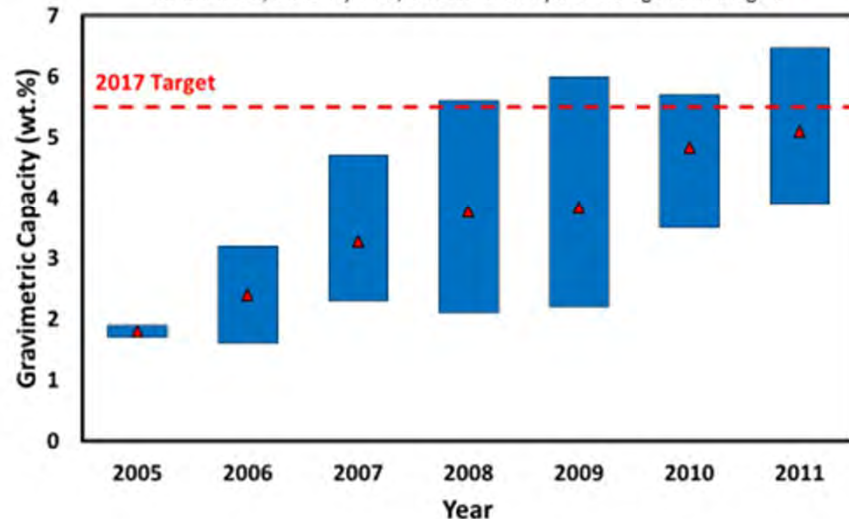
[1] Cost ranges for each pathway are shown in 2007\$ based on high-volume projections from H2A analyses, reflecting variability in major feedstock pricing and a bounded range for capital cost estimates.
 [2] Costs include total cost of production and delivery (dispensed, untaxed). Forecourt compression, storage and dispensing added an additional \$1.82 for distributed technologies, \$2.61 was added as the price of delivery to central technologies. All delivery costs were based on the Hydrogen Pathways Technical Report (NREL, 2009).
 [3] Analysis of projected costs for natural gas reforming indicated that the threshold cost can be achieved with current technologies or with incremental improvements made by industry. FCTP funding of natural gas reforming projects was completed in 2008.



Projected Capacities for Complete 5.6-kg H₂ Storage Systems

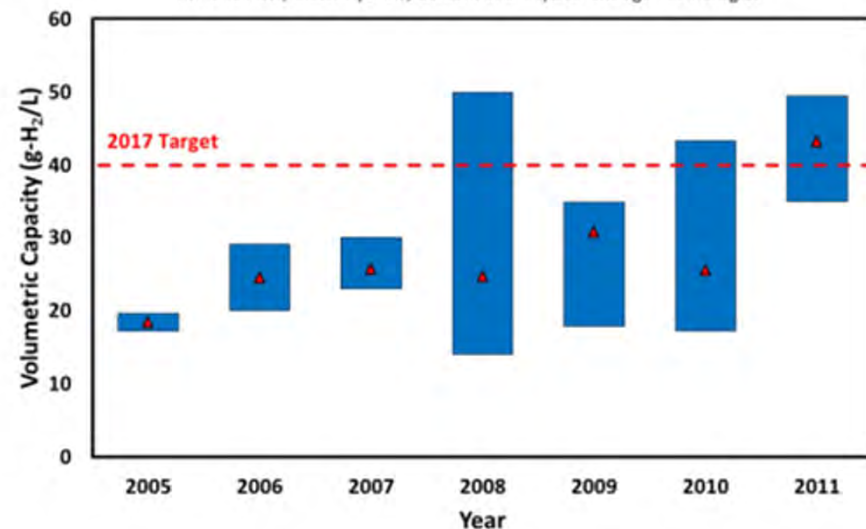
Projected Ranges of System Gravimetric Storage Capacity

For Chemical, Metal Hydride, Sorbent and Physical Storage Technologies



Projected Ranges of System Volumetric Storage Capacity

For Chemical, Metal Hydride, Sorbent and Physical Storage Technologies



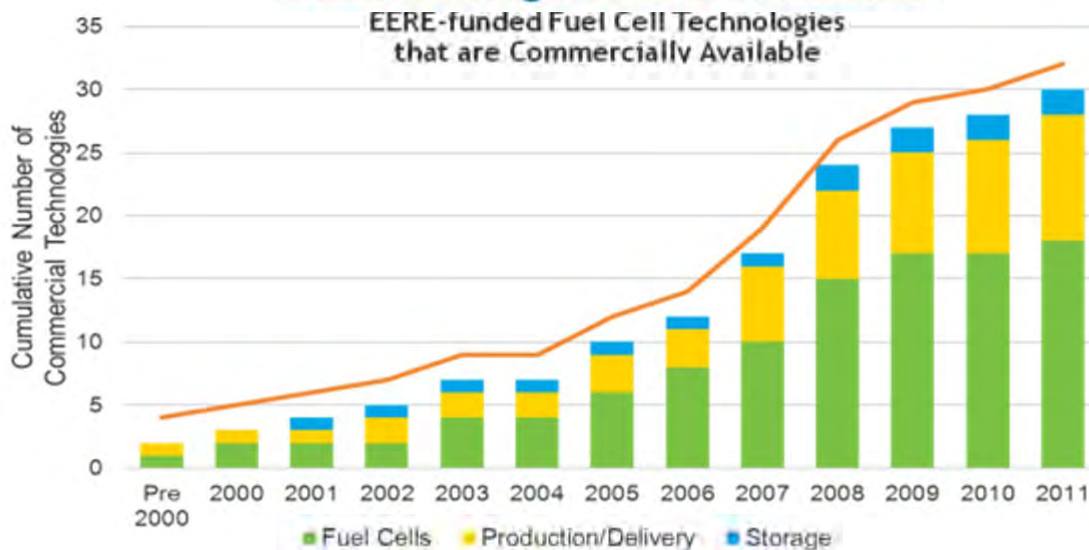
Progress is being made, but no technology meets all targets simultaneously.

- Bars represent the capacity range of technologies modeled in the given year, overall average for all technologies analyzed indicated.
- Projections performed by Argonne National Laboratory using the best available materials data and engineering analysis at the time of modeling.

H₂ Fuel Cell Technologies are being commercialized!

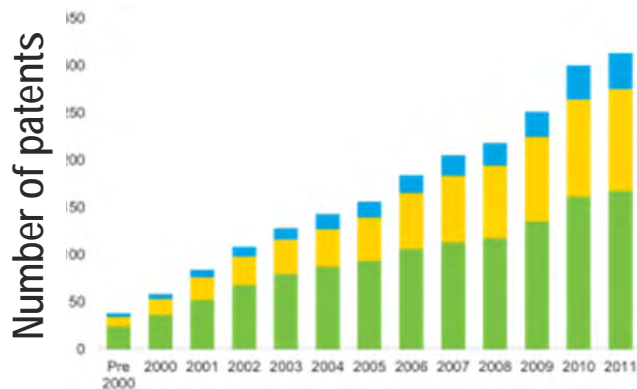
DOE funding has led to 313 patents, ~30 commercial technologies and >60 emerging technologies.
DOE's Impact: ~\$70M in funding for specific projects was tracked – and found to have led to nearly \$200M in industry investment and revenues.

Accelerating Commercialization



Source: Pacific Northwest National Laboratory

http://www1.eere.energy.gov/hydrogenandfuelcells/pdfs/pathways_success_hfcit.pdf



>310 PATENTS resulting from EERE-funded R&D:

- Includes technologies for hydrogen production and delivery, hydrogen storage, and fuel cells

http://www1.eere.energy.gov/hydrogenandfuelcells/pdfs/pathways_2011.pdf

Examples

3M

Proton Energy Systems

BASF Catalysts LLC

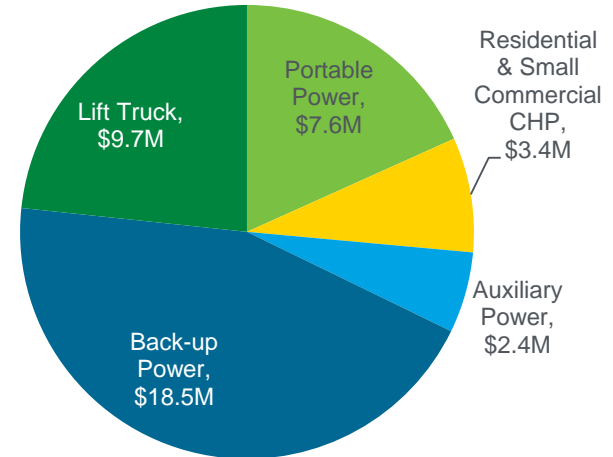
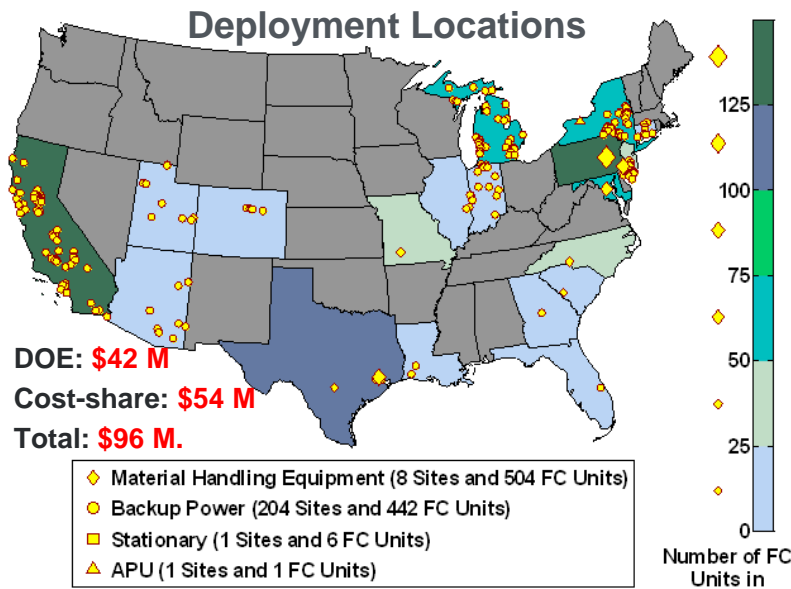
DuPont

Quantum Technologies

Dynalene, Inc.

Market Transformation – Addressing Market Barriers

Deployments help ensure continued technology utilization growth and catalyze market penetration while providing data and lessons learned.



ARRA Deployment Status – August 2011

Fuel Cell Application	Operational Fuel Cells	Total Fuel Cells Planned
Backup Power	371	539
Material Handling	467	504
Stationary	2	6
APU	0	4
Total	840	> 1,000



NREL ARRA Data Collection Snapshot

ARRA Material Handling Equipment Data	As of 9/30/2011
Hydrogen Dispensed	>51,500 kg
Hydrogen Fills	>88,000
Hours Accumulated	>380,000 hrs

MORE >3,000 ADDITIONAL FUEL CELL LIFT TRUCKS PLANNED with NO DOE funding

I wish to thank:

- My colleagues in the DOE Fuel Cell Technology Program;
- All the researchers whose work I borrowed from for my presentation and whom are too numerous to list individually here;
- **And especially the conference organizers for the invitation and you for listening!**

DOE Hydrogen Storage Team

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Thank you

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